

Towards
a high fidelity numerical algorithm
for
compressible multiphase flows

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Outline

State-of-the-art **relaxation models** for compressible multiphase flow with **cavitation** including phase transition take the form:

$$\partial_t \mathbf{q} + \operatorname{div} \mathbf{F}(\mathbf{q}) + \Pi(\mathbf{q}, \nabla \mathbf{q}) = \psi_p(\mathbf{q}) + \psi_{\mathbf{u}}(\mathbf{q}) + \psi_T(\mathbf{q}) + \psi_{pTg}(\mathbf{q}) + \dots$$

Model is approximated by **fractional-step** method:

1. **Homogeneous hyperbolic** step

$$\partial_t \mathbf{q} + \operatorname{div} \mathbf{F}(\mathbf{q}) + \Pi(\mathbf{q}, \nabla \mathbf{q}) = 0$$

2. **Source-term relaxation** step

$$\partial_t \mathbf{q} = \psi_p(\mathbf{q}) + \psi_{\mathbf{u}}(\mathbf{q}) + \psi_T(\mathbf{q}) + \psi_{pTg}(\mathbf{q}) + \dots$$

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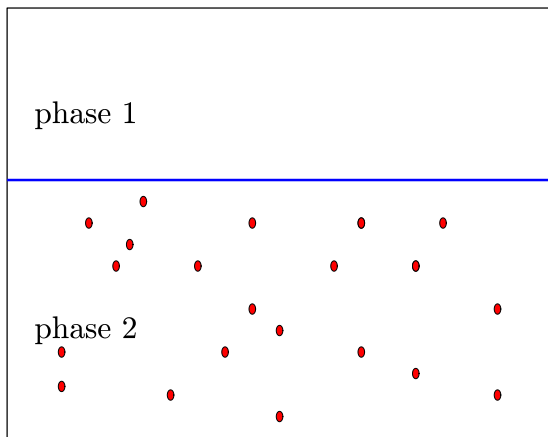
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Aim: **Discuss arbitrary-rate relaxation method for Step 2**

Compressible barotropic 2-phase, 2-component flow

Model problem: Bubbly liquid with interface



Compressible barotropic 2-phase, 2-component flow

L.-R. Plumerault (2009) proposed

$$\partial_t (\alpha_1 \rho_1) + \operatorname{div} (\alpha_1 \rho_1 \mathbf{u}) = 0 \quad (1a)$$

$$\partial_t (\alpha_2 \rho_2) + \operatorname{div} (\alpha_2 \rho_2 \mathbf{u}) = 0 \quad (1b)$$

$$\partial_t (\alpha_2 \rho_2 y_1) + \operatorname{div} (\alpha_2 \rho_2 y_1 \mathbf{u}) = 0 \quad (1c)$$

$$\partial_t (\rho \mathbf{u}) + \operatorname{div} (\rho \mathbf{u} \otimes \mathbf{u}) + \nabla p = 0 \quad (1d)$$

- Density-mixture conditions:

$$\rho = \alpha_1 \rho_1 + \alpha_2 \rho_2, \quad \rho_2 = \beta_1 \rho_{2,1} + \beta_2 \rho_{2,2}$$

- Saturation conditions for phase α_j & component β_k :

$$\alpha_1 + \alpha_2 = 1, \quad \beta_1 + \beta_2 = 1$$

- Mass fraction for phase Y_j & component y_k :

$$Y_1 + Y_2 = 1, \quad y_1 + y_2 = 1, \quad Y_j = \frac{\alpha_j \rho_j}{\rho}, \quad y_j = \frac{\beta_j \rho_{2,j}}{\rho_2}$$

- Pressure-mixture condition:

$$p = \alpha_1 p_1 + \alpha_2 p_2, \quad p_2 = \beta_1 p_{2,1} + \beta_2 p_{2,2}$$

- Model closure (pressure relaxation)

1. Pressure equilibrium for multicomponent

$$p_{2,1}(\rho_{2,1}) = p_{2,2}(\rho_{2,2}) = p_2$$

2. Pressure equilibrium for multiphase

$$p_1 = p_2$$

- Wood's sound speed for (phase 2) multicomponent mixture

$$\frac{1}{\rho_2 c_2^2} = \frac{\beta_1}{\rho_{2,1} c_{2,1}^2} + \frac{\beta_2}{\rho_{2,2} c_{2,2}^2}$$

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- Murnaghan isentropic EOS for p_k ,

$$p_k(\rho_k) = \left(p_{0,k} + \frac{K_{0S,k}}{K'_{0S,k}} \right) \left(\frac{\rho_k}{\rho_{0,k}} \right)^{K'_{0S,k}} - \frac{K_{0S,k}}{K'_{0S,k}} \quad (2)$$

Compressible barotropic 2-phase, 2-component flow

Model equations in **relaxation** (pressure nonequilibrium) form are:

$$\partial_t (\alpha_1 \rho_1) + \operatorname{div} (\alpha_1 \rho_1 \mathbf{u}) = 0 \quad (3a)$$

$$\partial_t (\alpha_2 \rho_2) + \operatorname{div} (\alpha_2 \rho_2 \mathbf{u}) = 0 \quad (3b)$$

$$\partial_t (\alpha_2 \rho_2 y_1) + \operatorname{div} (\alpha_2 \rho_2 y_1 \mathbf{u}) = 0 \quad (3c)$$

$$\partial_t (\rho \mathbf{u}) + \operatorname{div} (\rho \mathbf{u} \otimes \mathbf{u}) + \nabla (\alpha_1 p_1 + \alpha_2 p_2) = 0 \quad (3d)$$

$$\partial_t \alpha_1 + \mathbf{u} \cdot \nabla \alpha_1 = \mu (p_1 - p_2) \quad (3e)$$

$$\partial_t \alpha_2 + \mathbf{u} \cdot \nabla \alpha_2 = \mu (p_2 - p_1) \quad (3f)$$

Written (3) in compact form, we have

$$\partial_t \mathbf{q} + \operatorname{div} \mathbf{F}(\mathbf{q}) + \Pi(\mathbf{q}, \nabla \mathbf{q}) = \psi_p(\mathbf{q}) \quad (4)$$

Assume relaxation constant μ is known a priori. In pressure (mechanical) relaxation step, from (3) we have

$$\partial_t \mathbf{q} = \psi_p(\mathbf{q}) \quad (5a)$$

$$\mathbf{q} = [\alpha_1 \rho_1, \alpha_2 \rho_2, \alpha_2 \rho_2 y_1, \rho \mathbf{u}, \alpha_1, \alpha_2]^T \quad (5b)$$

$$\psi(\mathbf{q}) = [0, 0, 0, 0, \mu(p_1 - p_2), \mu(p_2 - p_1)]^T \quad (5c)$$

In exponential mechanical relaxation method, as in J.-M. Hérard & coworkers, in addition to (5), we introduce

$$\partial_t p_1 = -\frac{\rho_1 c_1^2}{\alpha_1} \partial_t \alpha_1 = -\mu \frac{\rho_1 c_1^2}{\alpha_1} (p_1 - p_2)$$

$$\partial_t p_2 = -\frac{\rho_2 c_2^2}{\alpha_2} \partial_t \alpha_2 = -\mu \frac{\rho_2 c_2^2}{\alpha_2} (p_2 - p_1)$$

Let $\Delta p = p_1 - p_2$. We have ODE for Δp :

$$\partial_t \Delta p = -\mu \left(\frac{\rho_1 c_1^2}{\alpha_1} + \frac{\rho_2 c_2^2}{\alpha_2} \right) \Delta p$$

With initial Δp^0 , we find **exact** solution of Δp over Δt :

$$\Delta p^* = \Delta p^0 \exp \{ -\mu (Z_1 + Z_2) \Delta t \}, \quad Z_j = \rho_j c_j^2 / \alpha_j$$

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- Update volume fractions using Δp^* , where $\alpha_1^* + \alpha_2^* = 1$:

$$\alpha_1^* = \alpha_1^0 - (Z_1 + Z_2)^{-1} (\Delta p^* - \Delta p^0)$$

$$\alpha_2^* = \alpha_2^0 + (Z_1 + Z_2)^{-1} (\Delta p^* - \Delta p^0)$$

If positivity condition $\alpha_k^* \in (0, 1)$, $k = 1, 2$ is satisfied; **we are done**.

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$$\frac{\alpha_1 \rho_1}{\rho_1 (p_1)} + \frac{\alpha_2 \rho_2}{\rho_2 (p_1 - \Delta p^*)} = 1$$

for p_1^* & set $p_2^* = p_1^* - \Delta p^*$ with **arbitrary rate constant** μ

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If $\mu \rightarrow \infty$ (instantaneous relaxation), we have $\Delta p^* \rightarrow 0$, yielding equilibrium pressure $p_1^* = p_2^* = p^*$

Compressible barotropic 3-phase, 2-component flow

Model equations in non-equilibrium form:

$$\partial_t (\alpha_1 \rho_1) + \operatorname{div} (\alpha_1 \rho_1 \mathbf{u}) = 0 \quad (6a)$$

$$\partial_t (\alpha_2 \rho_2) + \operatorname{div} (\alpha_2 \rho_2 \mathbf{u}) = 0 \quad (6b)$$

$$\partial_t (\alpha_3 \rho_3) + \operatorname{div} (\alpha_3 \rho_3 \mathbf{u}) = 0 \quad (6c)$$

$$\partial_t (\alpha_3 \rho_3 y_1) + \operatorname{div} (\alpha_3 \rho_3 y_1 \mathbf{u}) = 0 \quad (6d)$$

$$\partial_t (\rho \mathbf{u}) + \operatorname{div} (\rho \mathbf{u} \otimes \mathbf{u}) + \nabla (\alpha_1 p_1 + \alpha_2 p_2 + \alpha_3 p_3) = 0 \quad (6e)$$

$$\partial_t \alpha_1 + \mathbf{u} \cdot \nabla \alpha_1 = \mu_{12} (p_1 - p_2) + \mu_{13} (p_1 - p_3) \quad (6f)$$

$$\partial_t \alpha_2 + \mathbf{u} \cdot \nabla \alpha_2 = \mu_{21} (p_2 - p_1) + \mu_{23} (p_2 - p_3) \quad (6g)$$

$$\partial_t \alpha_3 + \mathbf{u} \cdot \nabla \alpha_3 = \mu_{31} (p_3 - p_1) + \mu_{32} (p_3 - p_2) \quad (6h)$$

- Density-mixture conditions:

$$\rho = \alpha_1 \rho_1 + \alpha_2 \rho_2 + \alpha_3 \rho_3, \quad \rho_3 = \beta_1 \rho_{3,1} + \beta_2 \rho_{3,2}$$

- Saturation conditions for phase α_j & component β_k :

$$\alpha_1 + \alpha_2 + \alpha_3 = 1, \quad \beta_1 + \beta_2 = 1$$

- Mass fraction for phase Y_j & component y_k :

$$Y_1 + Y_2 + Y_3 = 1, \quad y_1 + y_2 = 1, \quad Y_j = \frac{\alpha_j \rho_j}{\rho}, \quad y_j = \frac{\beta_j \rho_{3,j}}{\rho_2}$$

Barotropic 3-phase model: pressure relaxation

Assume relaxation constant $\mu_{ij} = \mu_{ji}$, $\forall i, j$ is known a priori.
In pressure relaxation step, from (6) we have

$$\partial_t (\alpha_k \rho_k) = 0, \quad k = 1, 2, 3$$

$$\partial_t (\alpha_3 \rho_3 y_1) = 0, \quad \partial_t (\rho \mathbf{u}) = 0$$

$$\partial_t \alpha_1 = \mu_{12} (p_1 - p_2) + \mu_{13} (p_1 - p_3)$$

$$\partial_t \alpha_2 = \mu_{12} (p_2 - p_1) + \mu_{23} (p_2 - p_3)$$

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In exponential relaxation method, if we use $\Delta p_{12} = p_1 - p_2$, $\Delta p_{13} = p_1 - p_3$, we obtain ODEs for Δp_{12} , Δp_{13} :

$$\begin{aligned}\partial_t \begin{bmatrix} \Delta p_{12} \\ \Delta p_{13} \end{bmatrix} &= -\mathcal{A} \begin{bmatrix} \Delta p_{12} \\ \Delta p_{13} \end{bmatrix} \\ \mathcal{A} &= \begin{bmatrix} \mu_{12} Z_1 + (\mu_{12} + \mu_{23}) Z_2 & \mu_{13} Z_1 - \mu_{23} Z_2 \\ \mu_{12} Z_1 - \mu_{23} Z_3 & \mu_{13} Z_1 + (\mu_{13} + \mu_{23}) Z_3 \end{bmatrix}\end{aligned}$$

With initial $(\Delta p_{12}^0, \Delta p_{13}^0)$, exact solution of ODE over Δt is

$$\begin{bmatrix} \Delta p_{12} \\ \Delta p_{13} \end{bmatrix}^* = \exp\{-\mathcal{A}\Delta t\} \begin{bmatrix} \Delta p_{12} \\ \Delta p_{13} \end{bmatrix}^0$$

Eigenvalues of \mathcal{A} are $\lambda_{\pm} = \frac{1}{2} \left(\text{tr}(\mathcal{A}) \pm \sqrt{\text{tr}(\mathcal{A})^2 - 4\det(\mathcal{A})} \right)$

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- Update volume fractions using Δp_{12}^* & Δp_{13}^* ,

$$\partial_t \begin{bmatrix} \alpha_1 \\ \alpha_2 \\ \alpha_3 \end{bmatrix} = \mathcal{B} \begin{bmatrix} \Delta p_{12} \\ \Delta p_{13} \end{bmatrix}, \quad \mathcal{B} = \begin{bmatrix} \mu_{12} & \mu_{13} \\ -\mu_{12} - \mu_{23} & \mu_{23} \\ \mu_{23} & -\mu_{13} - \mu_{23} \end{bmatrix},$$

we have

$$\begin{bmatrix} \alpha_1^* \\ \alpha_2^* \\ \alpha_3^* \end{bmatrix} = \begin{bmatrix} \alpha_1^0 \\ \alpha_2^0 \\ \alpha_3^0 \end{bmatrix} - \mathcal{B}\mathcal{A} \begin{bmatrix} \Delta p_{12}^* - \Delta p_{12}^0 \\ \Delta p_{13}^* - \Delta p_{13}^0 \end{bmatrix}$$

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for p_1^* & set

$$p_2^* = p_1^* - \Delta p_{12}^*, \quad p_3^* = p_1^* - \Delta p_{13}^*$$

with **arbitrary rate constant** μ_{ij} , yielding phasic density ρ_1^* , ρ_2^* , ρ_3^* and volume fraction α_1^* , α_2^* , α_3^*

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If $\mu_{ij} \rightarrow \infty$ (instantaneous relaxation), we have $\Delta p_{12}^* \rightarrow 0$ & $\Delta p_{13}^* \rightarrow 0$, yielding equilibrium pressure $p_1^* = p_2^* = p_3^* = p^*$

Compressible barotropic multiphase flow: summary

If $\mu_{ij} = \mu$, ODE systems in exponential pressure relaxation method are

- 2-phase case

$$\partial_t \Delta p_{12} = -\mu [Z_1 + Z_2] \Delta p_{12}$$

- 3-phase case

$$\partial_t \begin{bmatrix} \Delta p_{12} \\ \Delta p_{13} \end{bmatrix} = -\mu \begin{bmatrix} Z_1 + 2Z_2 & Z_1 - Z_2 \\ Z_1 - Z_3 & Z_1 + 2Z_3 \end{bmatrix} \begin{bmatrix} \Delta p_{12} \\ \Delta p_{13} \end{bmatrix}$$

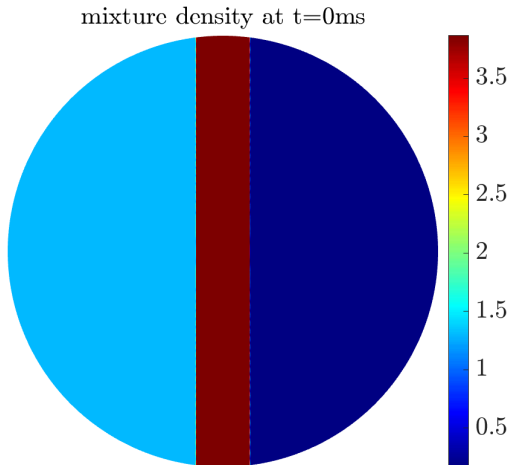
- 4-phase case

$$\partial_t \begin{bmatrix} \Delta p_{12} \\ \Delta p_{13} \\ \Delta p_{14} \end{bmatrix} = -\mu \begin{bmatrix} Z_1 + 3Z_2 & Z_1 - Z_2 & Z_1 - Z_2 \\ Z_1 - Z_3 & Z_1 + 3Z_3 & Z_1 - Z_3 \\ Z_1 - Z_4 & Z_1 - Z_4 & Z_1 + 3Z_4 \end{bmatrix} \begin{bmatrix} \Delta p_{12} \\ \Delta p_{13} \\ \Delta p_{14} \end{bmatrix}$$

Moving vessel problem: all gas 3-phase case

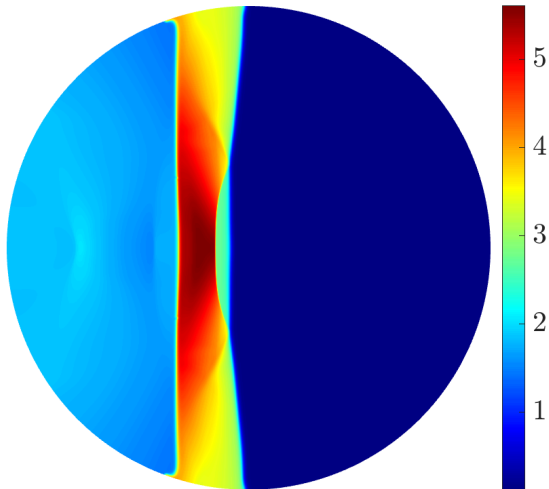
Moving velocity $\mathbf{u} = (-100, 0)$

EOS: $p_k(\rho_k) = p_{0,k} (\rho_k/\rho_{k,0})^{\gamma_k}$ $k = 1, 2, 3$



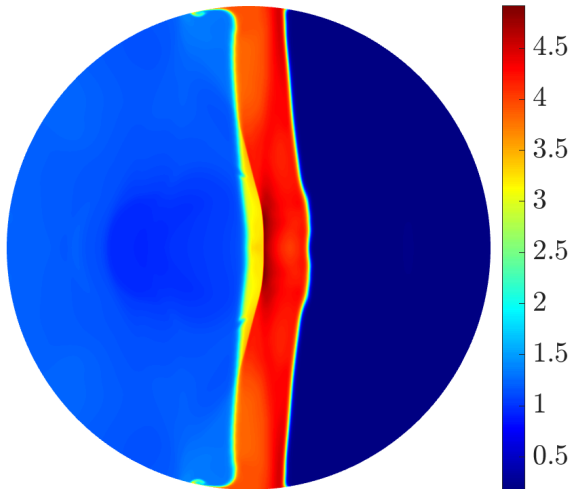
Moving vessel problem: all gas 3-phase case

mixture density at $t=2.5\text{ms}$



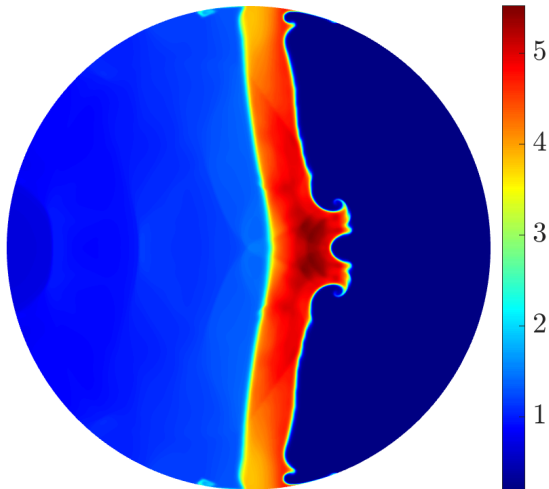
Moving vessel problem: all gas 3-phase case

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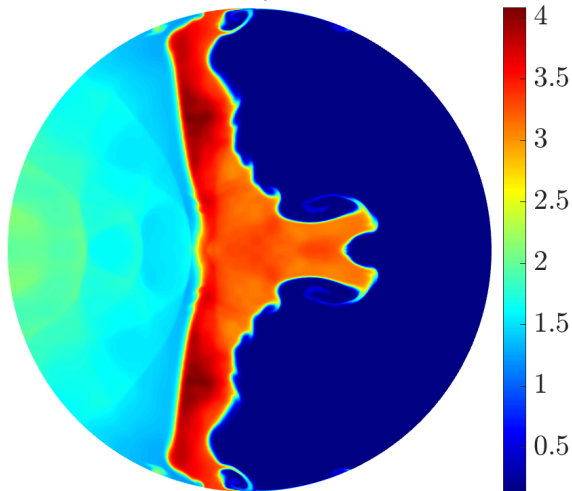
Moving vessel problem: all gas 3-phase case

mixture density at $t=7.5\text{ms}$

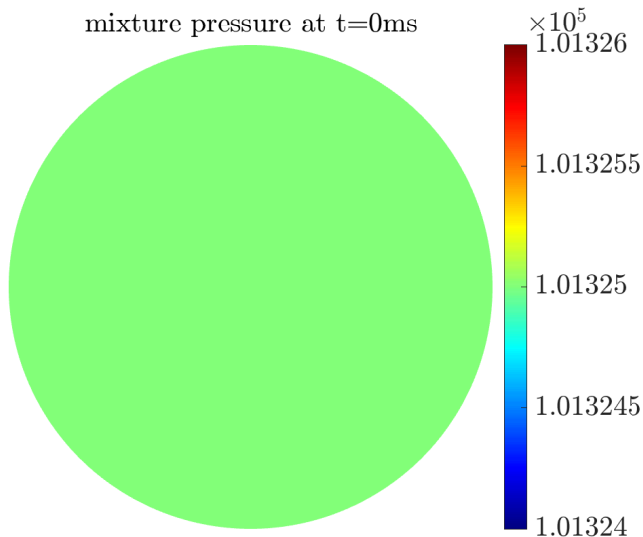


Moving vessel problem: all gas 3-phase case

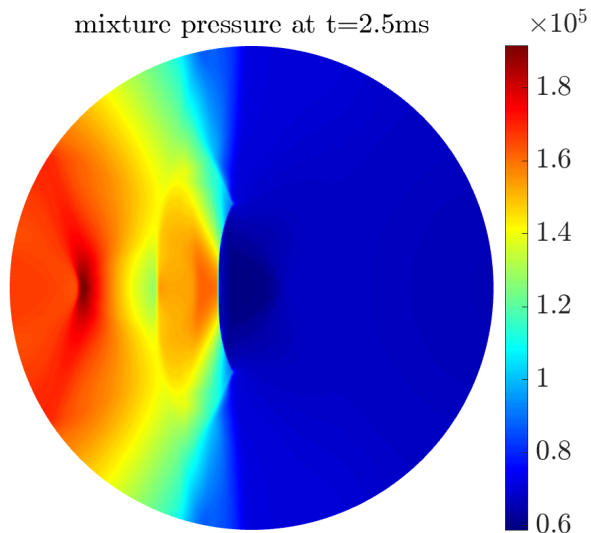
mixture density at $t=10\text{ms}$



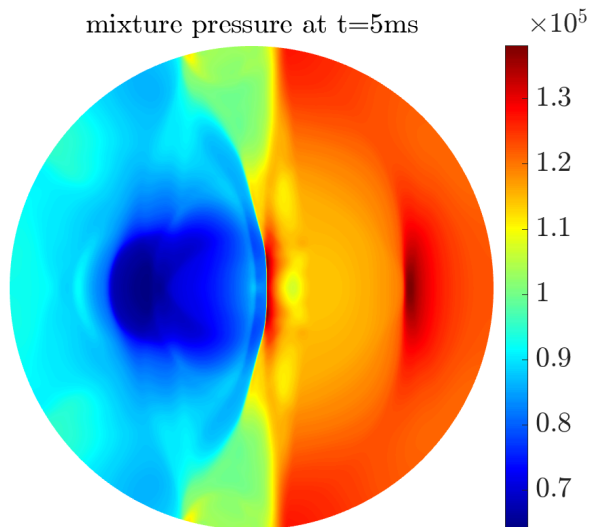
Moving vessel problem: all gas 3-phase case



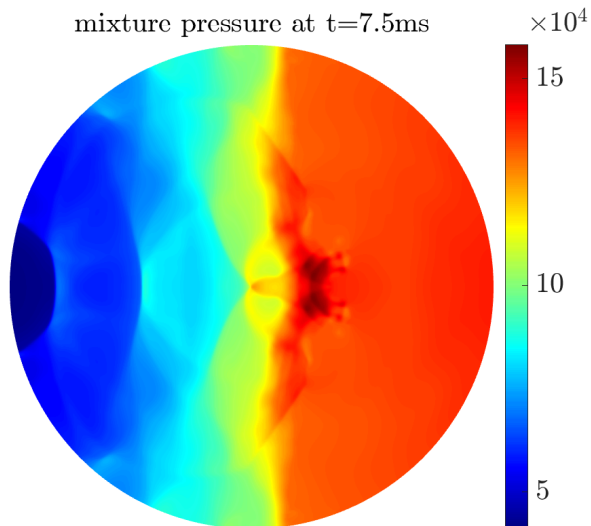
Moving vessel problem: all gas 3-phase case



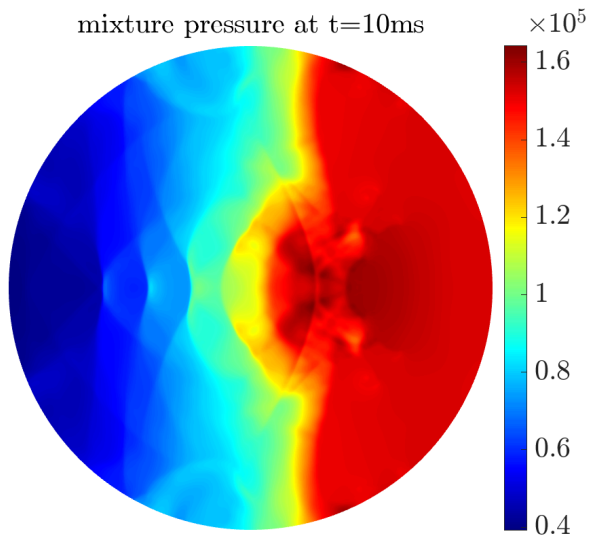
Moving vessel problem: all gas 3-phase case



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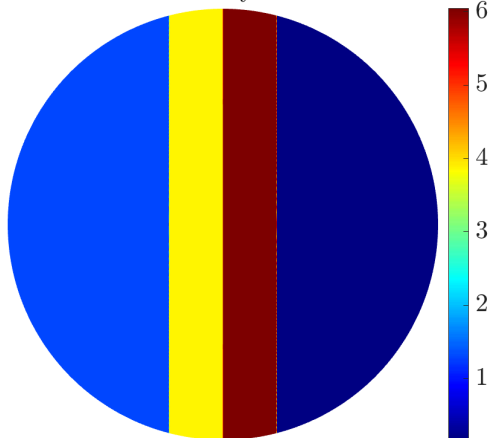


Moving vessel problem: all gas 4-phase case

Moving velocity $\mathbf{u} = (-100, 0)$

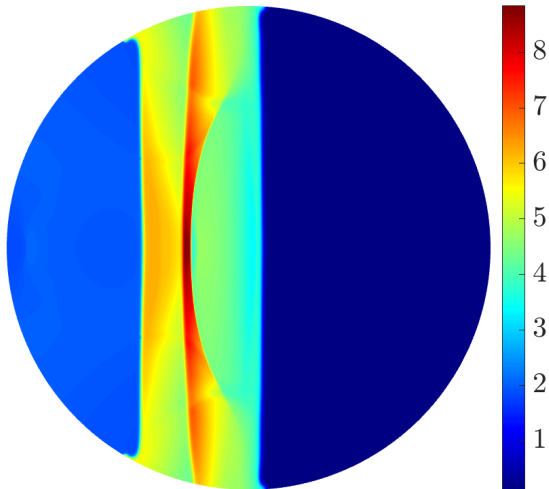
EOS: $p_k(\rho_k) = p_{0,k} (\rho_k/\rho_{k,0})^{\gamma_k}$ $k = 1, 2, 3, 4$

mixture density at $t=0\text{ms}$



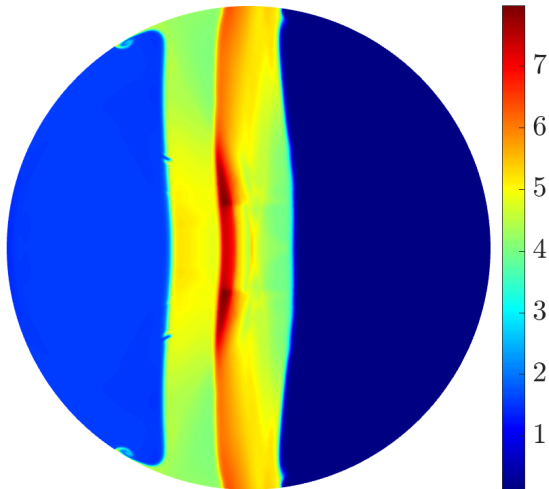
Moving vessel problem: all gas 4-phase case

mixture density at $t=2.5\text{ms}$



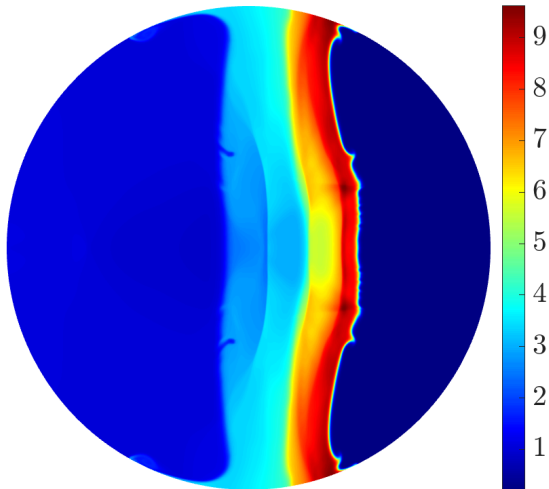
Moving vessel problem: all gas 4-phase case

mixture density at $t=5\text{ms}$



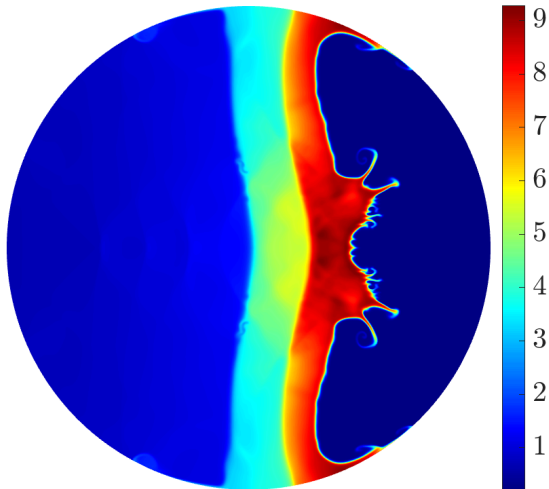
Moving vessel problem: all gas 4-phase case

mixture density at $t=7.5\text{ms}$

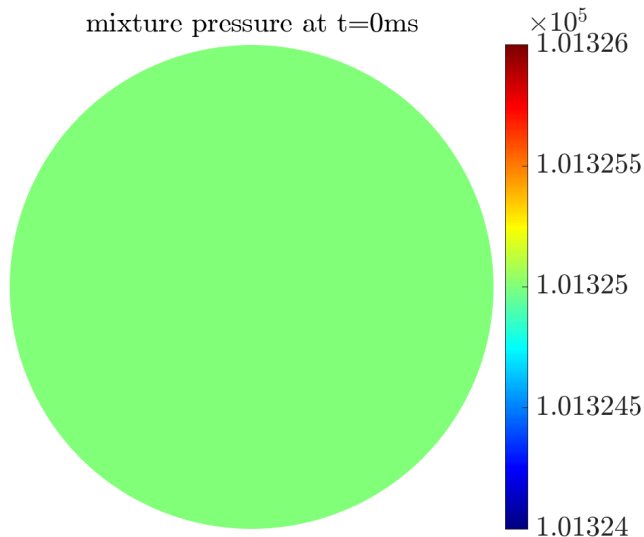


Moving vessel problem: all gas 4-phase case

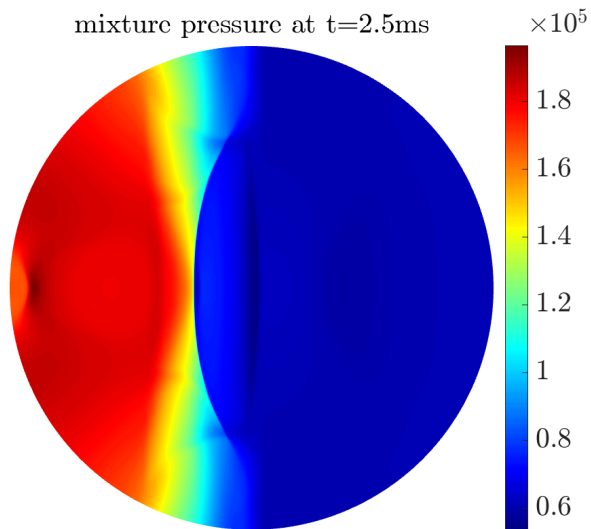
mixture density at $t=10\text{ms}$



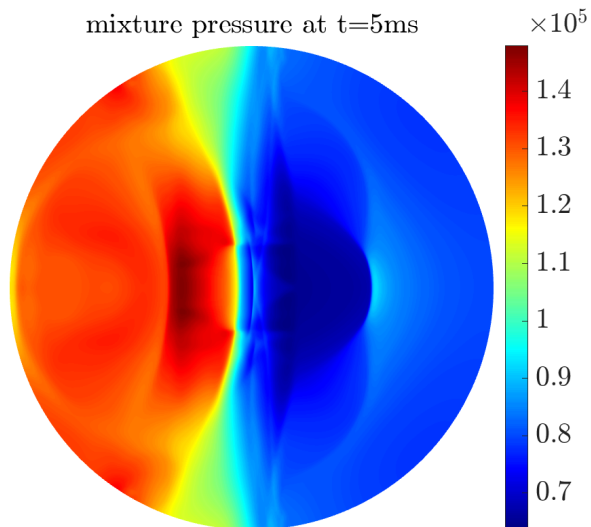
Moving vessel problem: all gas 4-phase case



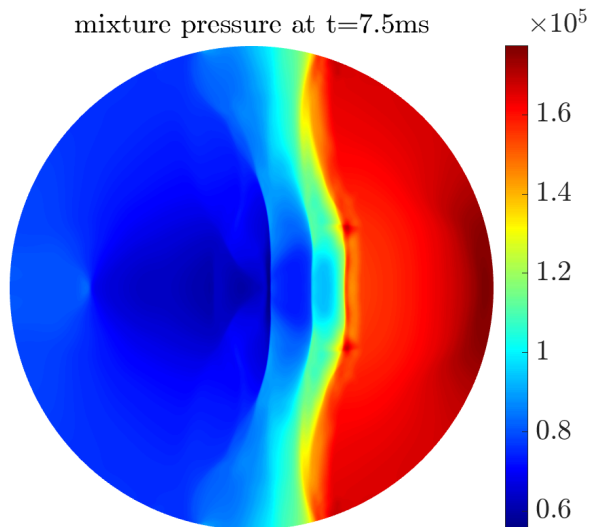
Moving vessel problem: all gas 4-phase case



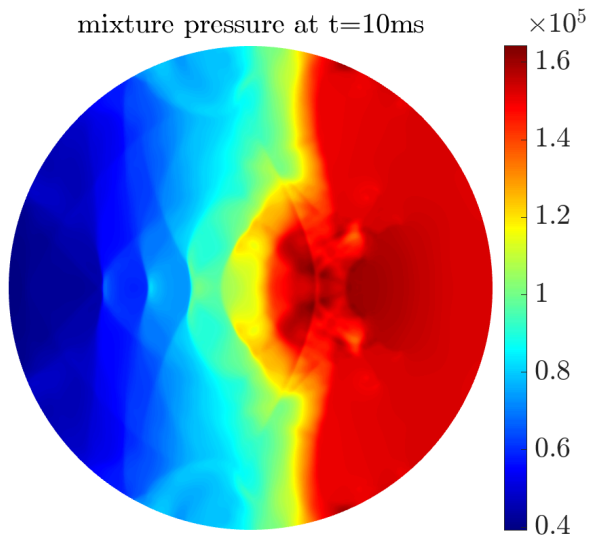
Moving vessel problem: all gas 4-phase case



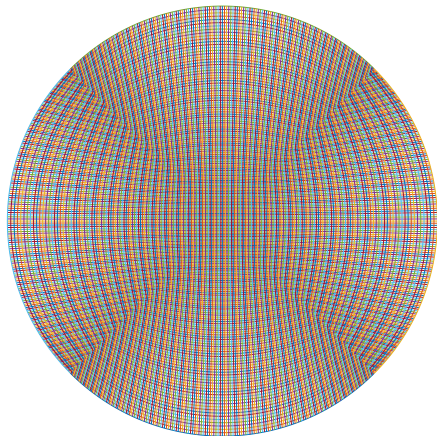
Moving vessel problem: all gas 4-phase case



Moving vessel problem: all gas 4-phase case



Moving vessel problem: mapped grid



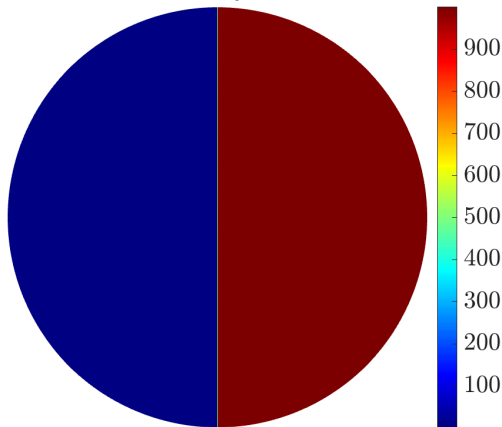
Moving vessel problem: gas-liquid case

Moving velocity $\mathbf{u} = (-100, 0)$

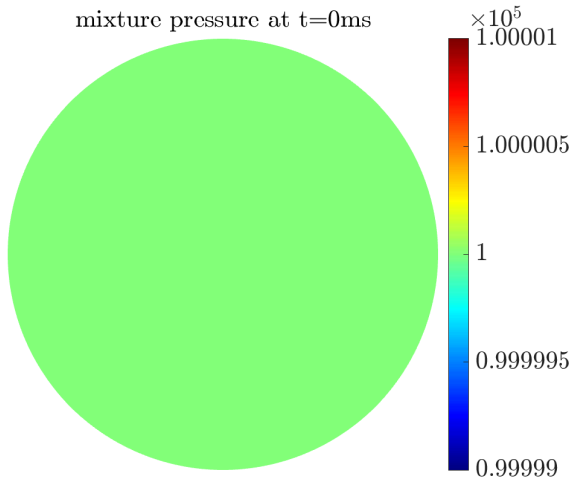
EOS for gas $p_1(\rho_1) = p_{0,1} (\rho_1/\rho_{1,0})^{\gamma_1}$ &

for liquid $p_2(\rho_2) = (p_{0,2} + \varpi_2) (\rho_2/\rho_{2,0})^{\gamma_2} + \varpi_2$

mixture density at $t=0\text{ms}$

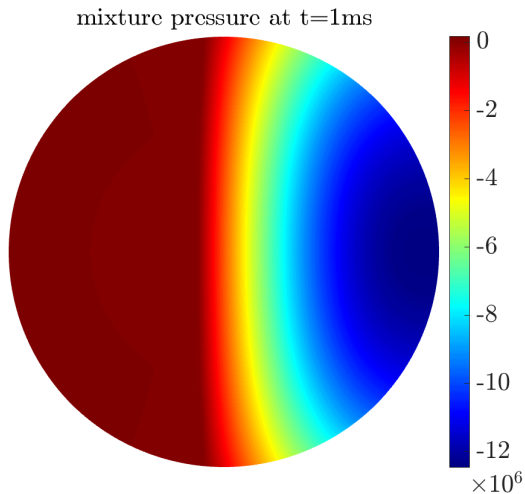


Moving vessel problem: gas-liquid case

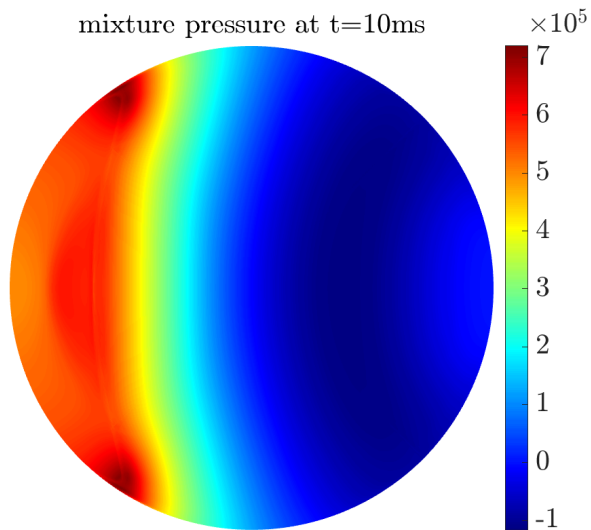


Moving vessel problem: gas-liquid case

Formation of negative pressure

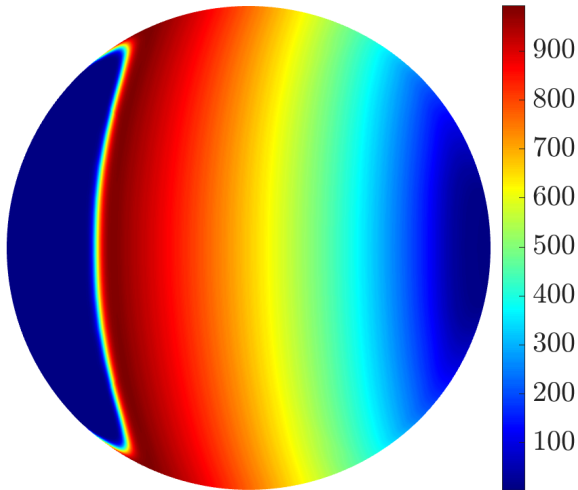


Moving vessel problem: gas-liquid case



Moving vessel problem: gas-liquid case

mixture density at $t=10\text{ms}$



With hope to achieve fast convergence for feasible phasic pressure p_k , for 3-phase flow, for example, one may choose Δ_k for $k = 1, 2, 3$, and solve saturation equation

$$\frac{\alpha_1 \rho_1}{\rho_1(\pi + \Delta_1)} + \frac{\alpha_2 \rho_2}{\rho_2(\pi + \Delta_2)} + \frac{\alpha_3 \rho_3}{\rho_3(\pi + \Delta_3)} = 1$$

for π . We then set

$$p_k = \pi + \Delta_k, \quad k = 1, 2, 3$$

Constraints for Δ_k are:

$$\Delta_1 - \Delta_2 = \Delta p_{12}, \quad \Delta_1 - \Delta_3 = \Delta p_{13}, \quad (7)$$

2 equations with 3 unknowns;

With hope to achieve **fast convergence for feasible** phasic pressure p_k , for 3-phase flow, for example, one may choose Δ_k for $k = 1, 2, 3$, and solve saturation equation

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2 equations with 3 unknowns; seek, for example, **minimum-norm solution** of (7)

$$\Delta_1 = \Delta p_{13}, \quad \Delta_2 = \Delta p_{13} - \Delta p_{12}, \quad \Delta_3 = 0$$

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2 equations with 3 unknowns; seek, for example, **minimum-norm solution** of (7)

$$\Delta_1 = \Delta p_{13}, \quad \Delta_2 = \Delta p_{13} - \Delta p_{12}, \quad \Delta_3 = 0$$

Relaxed solution depends strongly on initial condition from homogeneous hyperbolic step

Compressible non-barotropic 2-phase flow

Pelanti-Shyue (2014): 1-velocity phasic-total-energy model
without phase transition

$$\partial_t (\alpha_1 \rho_1) + \operatorname{div} (\alpha_1 \rho_1 \mathbf{u}) = 0 \quad (8a)$$

$$\partial_t (\alpha_2 \rho_2) + \operatorname{div} (\alpha_2 \rho_2 \mathbf{u}) = 0 \quad (8b)$$

$$\partial_t (\rho \mathbf{u}) + \operatorname{div} (\rho \mathbf{u} \otimes \mathbf{u}) + \nabla (\alpha_1 p_1 + \alpha_2 p_2) = 0 \quad (8c)$$

$$\partial_t (\alpha_1 \rho_1 E_1) + \operatorname{div} (\alpha_1 \rho_1 \mathbf{H}_1 \mathbf{u}) + \Upsilon = -\mu p_1 (p_1 - p_2) \quad (8d)$$

$$\partial_t (\alpha_2 \rho_2 E_2) + \operatorname{div} (\alpha_2 \rho_2 \mathbf{H}_2 \mathbf{u}) - \Upsilon = -\mu p_1 (p_2 - p_1) \quad (8e)$$

$$\partial_t \alpha_1 + \mathbf{u} \cdot \nabla \alpha_1 = \mu (p_1 - p_2) \quad (8f)$$

$$\partial_t \alpha_2 + \mathbf{u} \cdot \nabla \alpha_2 = \mu (p_2 - p_1) \quad (8g)$$

$$\Upsilon = \mathbf{u} \cdot [Y_1 \nabla (\alpha_2 p_2) - Y_2 \nabla (\alpha_1 p_1)], \quad H_k = E_k + \frac{p_k}{\rho_k}$$

Closure model: Mie-Grüneisen EOS for each p_k :

$$p_k(\rho_k, e_k) = p_{\text{ref},k}(\rho_k) + \frac{\Gamma_k}{\rho_k} (e_k - e_{\text{ref},k})$$

Non-barotropic 2-phase model: pressure relaxation

Assume relaxation constant μ is known a priori. In pressure relaxation step, from (8) we have

$$\partial_t (\alpha_1 \rho_1) = 0$$

$$\partial_t (\alpha_2 \rho_2) = 0$$

$$\partial_t (\rho \mathbf{u}) = 0$$

$$\partial_t (\alpha_1 \rho_1 E_1) = -\mu p_I (p_1 - p_2)$$

$$\partial_t (\alpha_2 \rho_2 E_2) = -\mu p_I (p_2 - p_1)$$

$$\partial_t \alpha_1 = \mu (p_1 - p_2)$$

$$\partial_t \alpha_2 = \mu (p_2 - p_1)$$

Phasic total energy equations can be simplified as

$$\partial_t (\alpha_1 \rho_1 e_1) = (\alpha_1 \rho_1) \partial_t e_1 = -\mu p_I (p_1 - p_2)$$

$$\partial_t (\alpha_2 \rho_2 e_2) = (\alpha_2 \rho_2) \partial_t e_2 = -\mu p_I (p_2 - p_1)$$

After simple algebraic manipulations, we have

$$\partial_t p_1 = -\mu \left(\frac{p_I - \rho_1^2 \partial_{p_1} e_1}{\alpha_1 \rho_1 \partial_{p_1} e_1} \right) (p_1 - p_2) = -\mu Z_1 (p_1 - p_2)$$

$$\partial_t p_2 = -\mu \left(\frac{p_I - \rho_2^2 \partial_{p_2} e_2 - p_I}{\alpha_2 \rho_2 \partial_{p_2} e_2} \right) (p_2 - p_1) = -\mu Z_2 (p_2 - p_1)$$

After simple algebraic manipulations, we have

$$\partial_t p_1 = -\mu \left(\frac{p_I - \rho_1^2 \partial_{\rho_1} e_1}{\alpha_1 \rho_1 \partial_{p_1} e_1} \right) (p_1 - p_2) = -\mu Z_1 (p_1 - p_2)$$

$$\partial_t p_2 = -\mu \left(\frac{p_I - \rho_2^2 \partial_{\rho_2} e_2 - p_I}{\alpha_2 \rho_2 \partial_{p_2} e_2} \right) (p_2 - p_1) = -\mu Z_2 (p_2 - p_1)$$

As before, in **exponential** relaxation method, we let

$\Delta p = p_1 - p_2$, and obtain ODE for Δp :

$$\partial_t \Delta p = -\mu (Z_1 + Z_2) \Delta p$$

With initial condition Δp^0 , **exact** solution of ODE over Δt is

$$\Delta p^* = \Delta p^0 \exp \{ -\mu (Z_1 + Z_2) \Delta t \}$$

After simple algebraic manipulations, we have

$$\partial_t p_1 = -\mu \left(\frac{p_I - \rho_1^2 \partial_{\rho_1} e_1}{\alpha_1 \rho_1 \partial_{p_1} e_1} \right) (p_1 - p_2) = -\mu Z_1 (p_1 - p_2)$$

$$\partial_t p_2 = -\mu \left(\frac{p_I - \rho_2^2 \partial_{\rho_2} e_2 - p_I}{\alpha_2 \rho_2 \partial_{p_2} e_2} \right) (p_2 - p_1) = -\mu Z_2 (p_2 - p_1)$$

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With initial condition Δp^0 , **exact** solution of ODE over Δt is

$$\Delta p^* = \Delta p^0 \exp \{ -\mu (Z_1 + Z_2) \Delta t \}$$

Stability condition of the method is $Z_1 + Z_2 \geq 0$; if not we set

$$\Delta p^* = 0$$

- Use exponential solution for α_k^* & p_k^* , $k = 1, 2$:

$$\alpha_1^* = \alpha_1^0 - (Z_1 + Z_2)^{-1} (\Delta p^* - \Delta p^0)$$

$$\alpha_2^* = \alpha_2^0 + (Z_1 + Z_2)^{-1} (\Delta p^* - \Delta p^0)$$

$$p_1^* = p_1^0 - Z_1 (\alpha_1^* - \alpha_1^0), \quad p_2^* = p_2^0 - Z_2 (\alpha_2^* - \alpha_2^0)$$

- Use exponential solution for α_k^* & p_k^* , $k = 1, 2$:

$$\alpha_1^* = \alpha_1^0 - (Z_1 + Z_2)^{-1} (\Delta p^* - \Delta p^0)$$

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$$p_1^* = p_1^0 - Z_1 (\alpha_1^* - \alpha_1^0), \quad p_2^* = p_2^0 - Z_2 (\alpha_2^* - \alpha_2^0)$$

If positivity condition $\alpha_k^* \in (0, 1)$, $k = 1, 2$ is satisfied; **we are done.**

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$$p_1^* = p_1^0 - Z_1 (\alpha_1^* - \alpha_1^0), \quad p_2^* = p_2^0 - Z_2 (\alpha_2^* - \alpha_2^0)$$

If positivity condition $\alpha_k^* \in (0, 1)$, $k = 1, 2$ is satisfied; **we are done**. Otherwise, we **modified** p_1^* & α_k^* using saturation condition proposed by Boukili & Hérard:

$$\frac{\alpha_1 \rho_1}{\rho_1(p_1, e_1)} + \frac{\alpha_2 \rho_2}{\rho_2(p_1 - \Delta p^*, e_2)} = 1;$$

for p_1^* & set $p_2^* = p_1^* - \Delta p^*$ with **arbitrary rate constant** μ

- Use exponential solution for α_k^* & p_k^* , $k = 1, 2$:

$$\alpha_1^* = \alpha_1^0 - (Z_1 + Z_2)^{-1} (\Delta p^* - \Delta p^0)$$

$$\alpha_2^* = \alpha_2^0 + (Z_1 + Z_2)^{-1} (\Delta p^* - \Delta p^0)$$

$$p_1^* = p_1^0 - Z_1 (\alpha_1^* - \alpha_1^0), \quad p_2^* = p_2^0 - Z_2 (\alpha_2^* - \alpha_2^0)$$

If positivity condition $\alpha_k^* \in (0, 1)$, $k = 1, 2$ is satisfied; **we are done**. Otherwise, we **modified** p_1^* & α_k^* using saturation condition proposed by Boukili & Hérard:

$$\frac{\alpha_1 \rho_1}{\rho_1(p_1, e_1)} + \frac{\alpha_2 \rho_2}{\rho_2(p_1 - \Delta p^*, e_2)} = 1;$$

for p_1^* & set $p_2^* = p_1^* - \Delta p^*$ with **arbitrary rate constant** μ

Pelanti (2022) considered $\mu \rightarrow \infty$, where **equilibrium pressure** p^* is updated from total internal energy

$$\sum_{k=1}^2 \alpha_k \rho_k e_k(\rho_k, p^*) = \sum_{k=1}^2 \alpha_k \rho_k E_k - \frac{1}{2} \rho \mathbf{u} \cdot \mathbf{u} = \text{constant}$$

Compressible non-barotropic multiphase flow

Pelanti-Shyue (2019): 1-velocity phasic-total-energy model
without phase transition

$$\partial_t(\alpha_k \rho_k) + \operatorname{div}(\alpha_k \rho_k \mathbf{u}) = 0, \quad k = 1, 2, \dots, N,$$

$$\partial_t(\rho \mathbf{u}) + \operatorname{div}(\rho \mathbf{u} \otimes \mathbf{u}) + \nabla \left(\sum_{k=1}^N \alpha_k p_k \right) = 0$$

$$\partial_t(\alpha_1 \rho_1 E_1) + \operatorname{div}(\alpha_1 \rho_1 H_1 \mathbf{u}) + \Upsilon_1 = - \sum_{j=1}^N p_{1j} \mathcal{P}_{1j}$$

$$\partial_t(\alpha_2 \rho_2 E_2) + \operatorname{div}(\alpha_2 \rho_2 H_2 \mathbf{u}) + \Upsilon_2 = - \sum_{j=1}^N p_{2j} \mathcal{P}_{2j}$$

$$\partial_t(\alpha_k \rho_k E_k) + \operatorname{div}(\alpha_k \rho_k H_k \mathbf{u}) + \Upsilon_k = - \sum_{j=1}^N p_{kj} \mathcal{P}_{kj}$$

$$\partial_t \alpha_k + \mathbf{u} \cdot \nabla \alpha_k = \sum_{j=1}^N \mathcal{P}_{kj}, \quad k = 1, 2, \dots, N$$

$$\Upsilon_k = \vec{u} \cdot \left(Y_k \nabla \left(\sum_{j=1}^N \alpha_j p_j \right) - \nabla(\alpha_k p_k) \right), \quad k = 1, 2, \dots, N$$

$$\mathcal{P}_{kj} = \mu_{kj} (p_k - p_j)$$

Non-barotropic multiphase flow: pressure relaxation

Assume $\mu_{kj} = \mu$, $p_{Ikj} = p_I$ for all k, j . ODE system for N -phase flow in exponential pressure relaxation method is

$$\partial_t \begin{bmatrix} \Delta p_{12} \\ \Delta p_{13} \\ \vdots \\ \Delta p_{1N} \end{bmatrix} = -\mu \mathcal{A} \begin{bmatrix} \Delta p_{12} \\ \Delta p_{13} \\ \vdots \\ \Delta p_{1N} \end{bmatrix}, \quad \text{with} \quad Z_k = \frac{p_I - \rho_k^2 \partial_{\rho_k} e_k}{\alpha_k \rho_k \partial_{p_k} e_k},$$

$$\mathcal{A} = \begin{bmatrix} Z_1 + (N-1)Z_2 & Z_1 - Z_2 & \cdots & Z_1 - Z_2 \\ Z_1 - Z_3 & Z_1 + (N-1)Z_3 & \cdots & Z_1 - Z_3 \\ \vdots & \ddots & \ddots & \vdots \\ Z_1 - Z_N & Z_1 - Z_N & \cdots & Z_1 + (N-1)Z_N \end{bmatrix}$$

With initial condition Δp_{1k}^0 , $k = 1, 2, \dots, N$ & arbitrary rate μ , exact solution of ODEs over Δt is

$$\begin{bmatrix} \Delta p_{12} \\ \Delta p_{13} \\ \vdots \\ \Delta p_{1N} \end{bmatrix}^* = \exp(-\mu \mathcal{A} \Delta t) \begin{bmatrix} \Delta p_{12} \\ \Delta p_{13} \\ \vdots \\ \Delta p_{1N} \end{bmatrix}^0$$

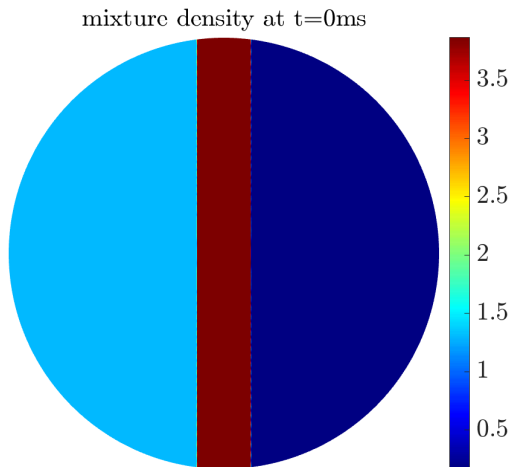
Stability condition for real part of eigenvalues of \mathcal{A} , $\text{Re}(\lambda_k(\mathcal{A})) \geq 0$ should be check first

We then continue determining phasic pressure p_k for $k = 1, 2, \dots, N$ using various techniques mentioned before

Moving vessel problem: all gas 3-phase case

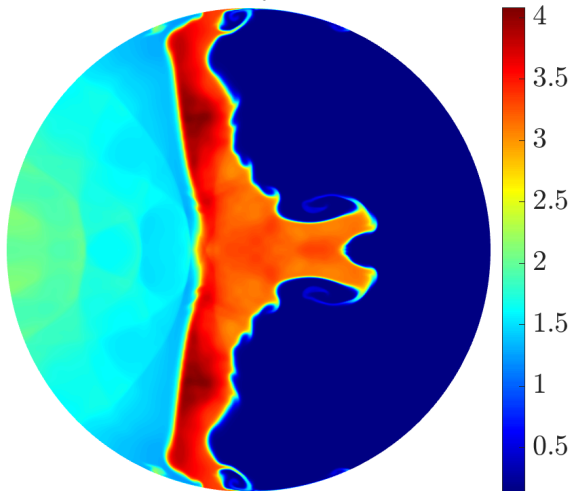
Moving velocity $\mathbf{u} = (-100, 0)$

EOS: $p_k(\rho_k, e_k) = (\gamma_k - 1)\rho_k e_k$, $k = 1, 2, 3$



Moving vessel problem: all gas 3-phase case

mixture density at $t=10\text{ms}$

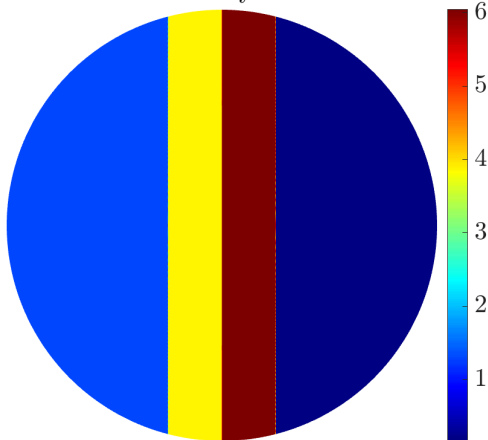


Moving vessel problem: all gas 4-phase case

Moving velocity $\mathbf{u} = (-100, 0)$

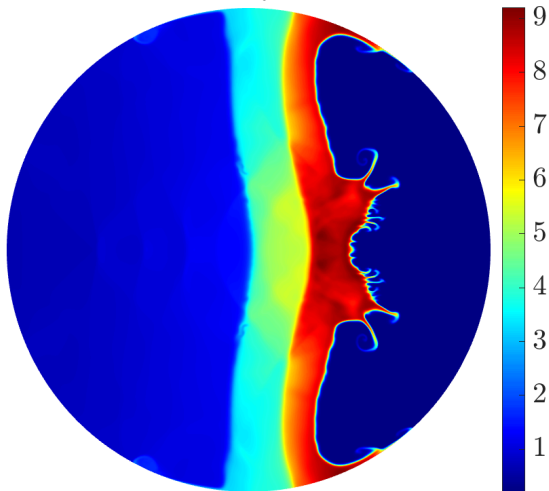
EOS: $p_k(\rho_k, e_k) = (\gamma_k - 1)\rho_k e_k$, $k = 1, 2, 3, 4$

mixture density at $t=0\text{ms}$



Moving vessel problem: all gas 4-phase case

mixture density at $t=10\text{ms}$



Cavitating Richtmyer-Meshkov: liquid-gas case

Moving velocity $\mathbf{u} = (-200, 0)$

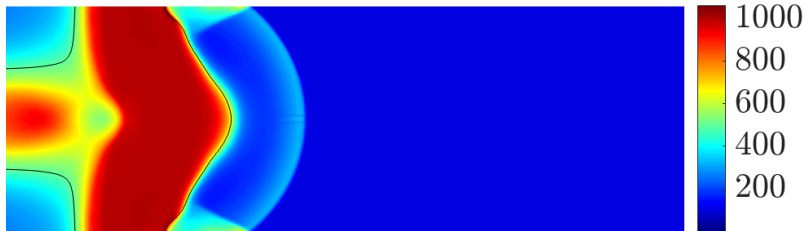
EOS: stiffened gas for gas & liquid

mixture density at $t=0\text{ms}$



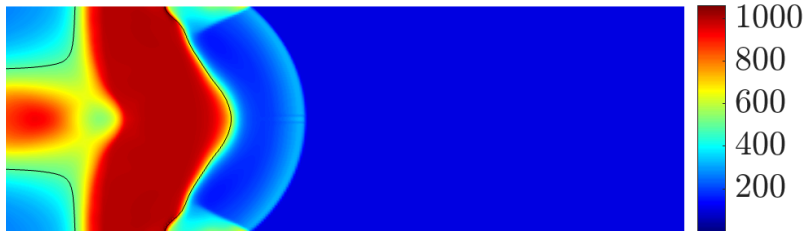
Cavitating Richtmyer-Meshkov: liquid-gas case

mixture density at $t=2\text{ms}$



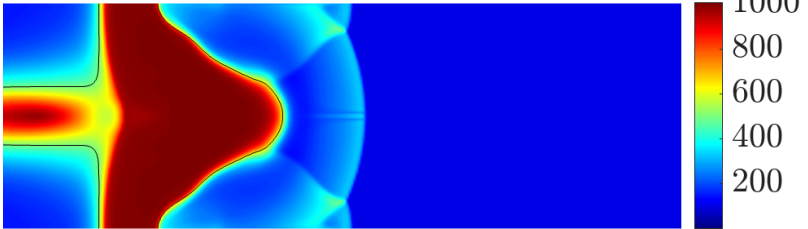
Cavitating Richtmyer-Meshkov: liquid-gas case

mixture density at $t=2\text{ms}$



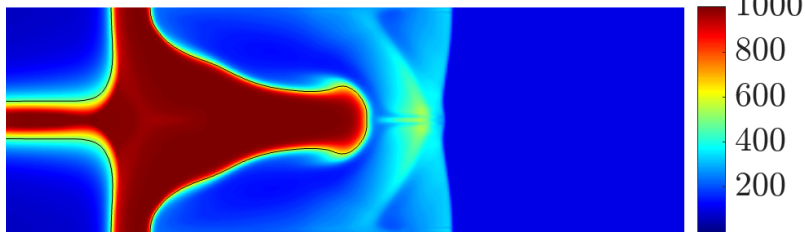
Cavitating Richtmyer-Meshkov: liquid-gas case

mixture density at $t=3.1\text{ms}$



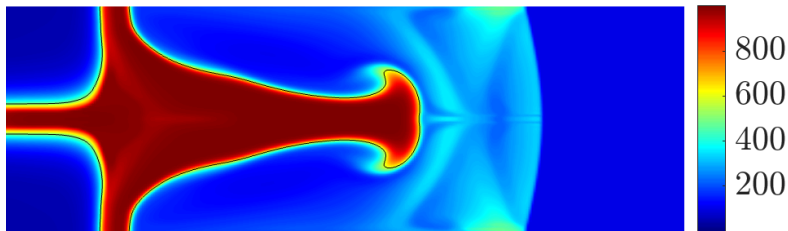
Cavitating Richtmyer-Meshkov: liquid-gas case

mixture density at $t=4.8\text{ms}$



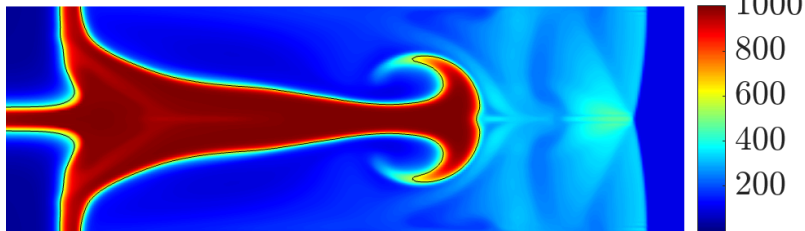
Cavitating Richtmyer-Meshkov: liquid-gas case

mixture density at $t=6.4\text{ms}$

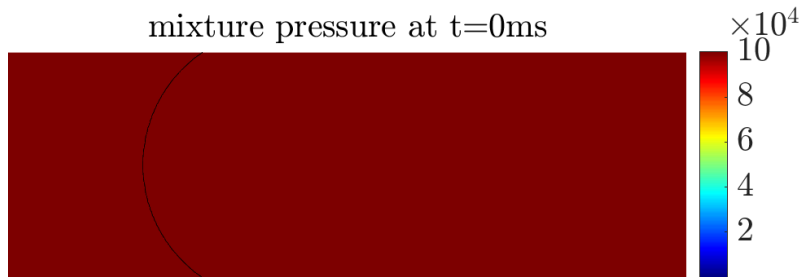


Cavitating Richtmyer-Meshkov: liquid-gas case

mixture density at $t=8.6\text{ms}$

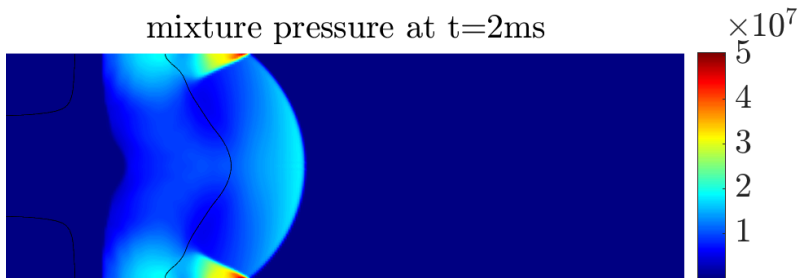


Cavitating Richtmyer-Meshkov: liquid-gas case



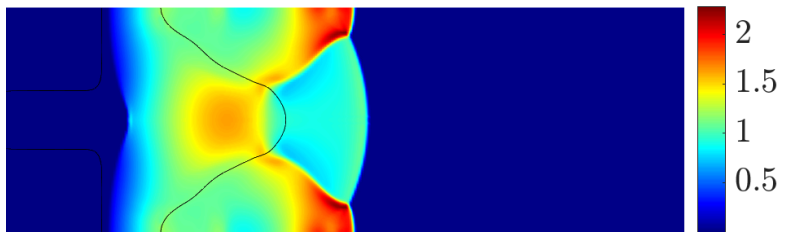
Cavitating Richtmyer-Meshkov: liquid-gas case

mixture pressure at $t=2\text{ms}$



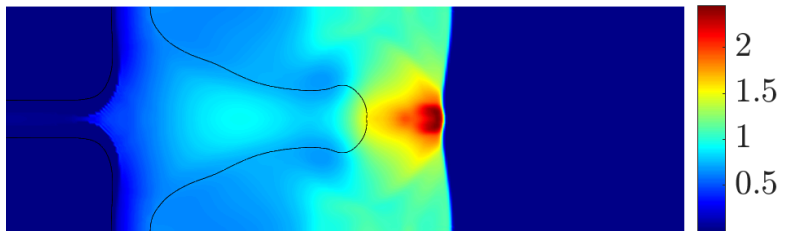
Cavitating Richtmyer-Meshkov: liquid-gas case

mixture pressure at $t=3.1\text{ms}$



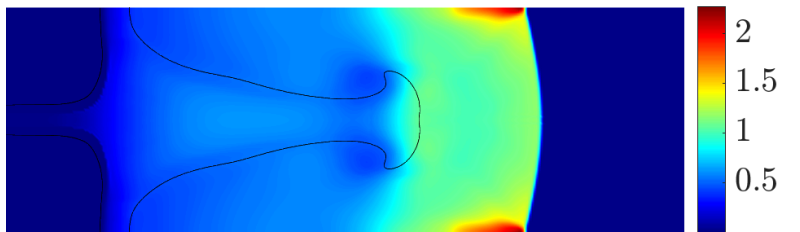
Cavitating Richtmyer-Meshkov: liquid-gas case

mixture pressure at $t=4.8\text{ms}$



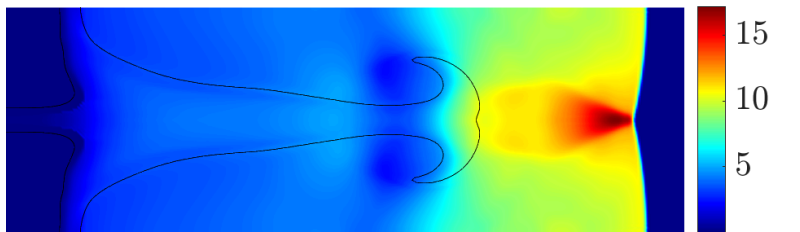
Cavitating Richtmyer-Meshkov: liquid-gas case

mixture pressure at $t=6.4\text{ms}$



Cavitating Richtmyer-Meshkov: liquid-gas case

mixture pressure at $t=8.6\text{ms}$



Hybrid barotropic & non-barotropic 2-phase flow

Suppose we model liquid-gas 2-phase flow by hybrid **barotropic** & **non-barotropic** EOS, & use reduced model equations:

$$\partial_t (\alpha_1 \rho_1) + \operatorname{div} (\alpha_1 \rho_1 \mathbf{u}) = 0 \quad (9a)$$

$$\partial_t (\alpha_2 \rho_2) + \operatorname{div} (\alpha_2 \rho_2 \mathbf{u}) = 0 \quad (9b)$$

$$\partial_t (\rho \mathbf{u}) + \operatorname{div} (\rho \mathbf{u} \otimes \mathbf{u}) + \nabla (\alpha_1 p_1 + \alpha_2 p_2) = 0 \quad (9c)$$

$$\partial_t (\alpha_2 \rho_2 E_2) + \operatorname{div} (\alpha_2 \rho_2 \mathbf{H}_2 \mathbf{u}) - \Upsilon = -\mu p_1 (p_2 - p_1) \quad (9d)$$

$$\partial_t \alpha_1 + \mathbf{u} \cdot \nabla \alpha_1 = \mu (p_1 - p_2) \quad (9e)$$

$$\partial_t \alpha_2 + \mathbf{u} \cdot \nabla \alpha_2 = \mu (p_2 - p_1) \quad (9f)$$

- Murnaghan isentropic EOS for phase 1

$$p_1(\rho_1) = \left(p_{0,1} + \frac{K_{0S,1}}{K'_{0S,1}} \right) \left(\frac{\rho_1}{\rho_{0,1}} \right)^{K'_{0S,1}} - \frac{K_{0S,1}}{K'_{0S,1}}$$

- Mie-Grüneisen EOS for phase 2

$$p_2(\rho_2, e_2) = p_{\text{ref},2}(\rho_2) + \frac{\Gamma_2}{\rho_2} (e_2 - e_{\text{ref},2})$$

As before, in **exponential** relaxation method, we let $\Delta p = p_1 - p_2$, and obtain ODE for Δp :

$$\partial_t \Delta p = -\mu (Z_1 + Z_2) \Delta p$$

with

$$Z_1 = \frac{\rho_1 c_1^2}{\alpha_1}$$

$$Z_2 = \frac{p_I - \rho_2^2 \partial_{\rho_2} e_2}{\alpha_2 \rho_2 \partial_{p_2} e_2}$$

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With initial condition Δp^0 , exact solution of ODE over Δt is

$$\Delta p^* = \Delta p^0 \exp \{ -\mu (Z_1 + Z_2) \Delta t \}$$

Model extension to multiphase flow can be formulated analogously

Cavitating Richtmyer-Meshkov: liquid-gas case

Moving velocity $\mathbf{u} = (-200, 0)$

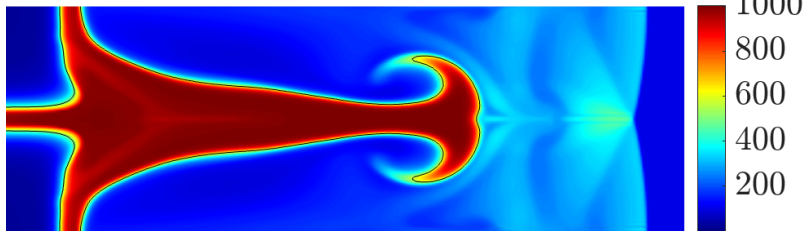
EOS: Tait for liquid & ideal for gas

mixture density at $t=0\text{ms}$



Cavitating Richtmyer-Meshkov: liquid-gas case

mixture density at $t=8.6\text{ms}$



Compressible multiphase flow with phase transition

Pelanti-Shyue (2019): 1-velocity model for compressible multiphase flow with liquid-vapor-gas phase transition is

$$\partial_t(\alpha_1\rho_1) + \operatorname{div}(\alpha_1\rho_1\mathbf{u}) = \mathcal{M}$$

$$\partial_t(\alpha_2\rho_2) + \operatorname{div}(\alpha_2\rho_2\mathbf{u}) = -\mathcal{M}$$

$$\partial_t(\alpha_k\rho_k) + \operatorname{div}(\alpha_k\rho_k\mathbf{u}) = 0, \quad k = 3, \dots, N$$

$$\partial_t(\rho\mathbf{u}) + \operatorname{div}(\rho\mathbf{u} \otimes \mathbf{u}) + \nabla \left(\sum_{k=1}^N \alpha_k p_k \right) = 0$$

$$\partial_t\alpha_k + \mathbf{u} \cdot \nabla\alpha_k = \sum_{j=1}^N \mathcal{P}_{kj}, \quad k = 1, 2, \dots, N$$

Here we have

$$\mathcal{P}_{kj} = \mu_{kj}(p_k - p_j) \quad (\text{volume transfer})$$

$$\mathcal{Q}_{kj} = \vartheta_{kj}(T_j - T_k) \quad (\text{heat transfer})$$

$$\mathcal{M} = \nu(g_2 - g_1) \quad (\text{mass transfer between liquid \& vapor phases})$$

$$g_k = h_k - T_k s_k \quad (\text{Gibbs free energy}), \quad h_k = e_k + p_k/\rho_k$$

Equations for total energy of each phase k are:

$$\partial_t(\alpha_1 \rho_1 E_1) + \text{div}(\alpha_1 \rho_1 \mathbf{H}_1 \mathbf{u}) + \Upsilon_1 = - \sum_{j=1}^N p_{11j} \mathcal{P}_{1j} + \sum_{j=1}^N \mathcal{Q}_{1j} + \left(g_I + \frac{|\mathbf{u}|^2}{2} \right) \mathcal{M}$$

$$\partial_t(\alpha_2 \rho_2 E_2) + \text{div}(\alpha_2 \rho_2 \mathbf{H}_2 \mathbf{u}) + \Upsilon_2 = - \sum_{j=1}^N p_{12j} \mathcal{P}_{2j} + \sum_{j=1}^N \mathcal{Q}_{2j} - \left(g_I + \frac{|\mathbf{u}|^2}{2} \right) \mathcal{M}$$

$$\partial_t(\alpha_k \rho_k E_k) + \text{div}(\alpha_k \rho_k \mathbf{H}_k \mathbf{u}) + \Upsilon_k = - \sum_{j=1}^N p_{Ikj} \mathcal{P}_{kj} + \sum_{j=1}^N \mathcal{Q}_{kj}, \quad k = 3, \dots, N$$

Closure model: Stiffened gas EOS (linear EOS)

Constitutive law: metastable fluid

Stiffened gas equation of state (SG EOS) with

- Pressure

$$p_k(e_k, \rho_k) = (\gamma_k - 1)e_k - \gamma_k \varpi_k - (\gamma_k - 1)\rho_k \eta_k$$

- Temperature

$$T_k(p_k, \rho_k) = \frac{p_k + \varpi_k}{(\gamma_k - 1)C_{V_k}\rho_k}$$

- Entropy

$$s_k(p_k, T_k) = C_{V_k} \log \frac{T_k^{\gamma_k}}{(p_k + \varpi_k)^{\gamma_k - 1}} + \eta'_k$$

- Helmholtz free energy $a_k = e_k - T_k s_k$
- Gibbs free energy $g_k = a_k + p_k V_k$

Metastable fluid: saturation curve

Assume two phases in chemical equilibrium with equal Gibbs free energies ($g_1 = g_2$), saturation curve is

$$\mathcal{G}(p, T) = A + \frac{B}{T} + C \log T + D \log(p + \varpi_1) - \log(p + \varpi_2) = 0$$

$$A = \frac{C_{p1} - C_{p2} + \eta'_2 - \eta'_1}{C_{p2} - C_{v2}}, \quad B = \frac{\eta_1 - \eta_2}{C_{p2} - C_{v2}}$$
$$C = \frac{C_{p2} - C_{p1}}{C_{p2} - C_{v2}}, \quad D = \frac{C_{p1} - C_{v1}}{C_{p2} - C_{v2}}$$

Metastable fluid: saturation curve

Assume two phases in chemical equilibrium with **equal Gibbs free energies** ($g_1 = g_2$), **saturation curve** is

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$$C = \frac{C_{p2} - C_{p1}}{C_{p2} - C_{v2}}, \quad D = \frac{C_{p1} - C_{v1}}{C_{p2} - C_{v2}}$$

or, from $dg_1 = dg_2$, we get **Clausius-Clapeyron** equation

$$\frac{dp(T)}{dT} = \frac{L_h}{T(v_2 - v_1)}$$

$L_h = T(s_2 - s_1)$: **latent heat of vaporization**

Thermo-chemical relaxation: instantaneous rate

Look for solution of ODEs in limits $\mu, \theta, \& \nu \rightarrow \infty$

$$\partial_t (\alpha_1 \rho_1) = \mathcal{M}$$

$$\partial_t (\alpha_2 \rho_2) = -\mathcal{M}$$

$$\partial_t (\alpha_k \rho_k) = 0, \quad k = 3, 4, \dots, N$$

$$\partial_t (\rho \mathbf{u}) = 0$$

$$\partial_t (\alpha_1 \rho_1 E_1) = - \sum_{j=1}^N p_{11j} \mathcal{P}_{1j} + \sum_{j=1}^N \mathcal{Q}_{1j} + \left(g_1 + \frac{|\mathbf{u}|^2}{2} \right) \mathcal{M}$$

$$\partial_t (\alpha_2 \rho_2 E_2) = - \sum_{j=1}^N p_{12j} \mathcal{P}_{2j} + \sum_{j=1}^N \mathcal{Q}_{2j} - \left(g_1 + \frac{|\mathbf{u}|^2}{2} \right) \mathcal{M}$$

$$\partial_t (\alpha_k \rho_k E_k) = - \sum_{j=1}^N p_{1kj} \mathcal{P}_{kj} + \sum_{j=1}^N \mathcal{Q}_{kj}, \quad k = 3, \dots, N$$

$$\partial_t \alpha_k = \sum_{j=1}^N \mathcal{P}_{kj}, \quad k = 1, 2, \dots, N$$

under **mechanical-thermal-chemical equilibrium** conditions

$$p_1 = p_2, \quad T_1 = T_2, \quad g_1 = g_2$$

Infinite-rate pTg relaxation: algebraic approach

In this case, states remain in equilibrium are

$$\rho = \rho_0, \quad \rho \mathbf{u} = \rho_0 \mathbf{u}_0, \quad \rho E = (\rho E)_0, \quad e = e_0,$$

& $\alpha_k \rho_k = (\alpha_k \rho_k)_0$, but $\alpha_k \rho_k \neq \alpha_{k0} \rho_{k0}$ & $Y_k \neq Y_{k0}$, $k = 1, 2$

Impose **mechanical-thermal-chemical equilibrium** to

1. Saturation condition for temperature

$$\mathcal{G}(p, T) = 0$$

2. Saturation condition for volume fraction

$$\frac{Y_1}{\rho_1(p, T)} + \frac{Y_2}{\rho_2(p, T)} = \frac{1}{\rho_0}$$

3. Equilibrium of internal energy

$$Y_1 e_1(p, T) + Y_2 e_2(p, T) = e_0$$

From saturation condition for temperature

$$\mathcal{G}(p, T) = 0$$

we get T in terms of p , while from

$$\frac{Y_1}{\rho_1(p, T)} + \frac{Y_2}{\rho_2(p, T)} = \frac{1}{\rho_0}$$

&

$$Y_1 e_1(p, T) + Y_2 e_2(p, T) = e_0$$

we obtain algebraic equation for p

$$Y_1 = \frac{1/\rho_2(p) - 1/\rho_0}{1/\rho_2(p) - 1/\rho_1(p)} = \frac{e_0 - e_2(p)}{e_1(p) - e_2(p)}$$

which is solved by iterative method

Instantaneous-rate pTg relaxation: remarks

- Having known Y_k & p, T can be solved from, e.g.,

$$Y_1 e_1(p, T) + Y_2 e_2(p, T) = e_0$$

yielding update ρ_k & α_k

- Feasibility of solutions, *i.e.*, positivity of physical quantities $\rho_k, \alpha_k, p,$ & T , for example
 - Employ **hybrid** method *i.e.*, combination of above method with differential-based approach (**not discuss** here), when it becomes necessary

Arbitrary-rate pTg relaxation: 2-phase flow case

Pelanti (2022): In [exponential thermo-chemical](#) relaxation method, we write ODEs governing chemical relaxation process as ODEs for $\Delta g = g_1 - g_2$:

$$\partial_t (\alpha_1 \rho_1) = -\nu (g_1 - g_2) \quad (10a)$$

$$\partial_t (\alpha_2 \rho_2) = -\nu (g_2 - g_1) \quad (10b)$$

$$\partial_t g_1 = -\nu \left(\frac{\mathcal{S}_p}{\rho_1} - s_1 \mathcal{S}_T \right) (g_1 - g_2) \quad (10c)$$

$$\partial_t g_2 = \nu \left(\frac{\mathcal{S}_p}{\rho_2} - s_2 \mathcal{S}_T \right) (g_2 - g_1) \quad (10d)$$

$$\partial_t \alpha_1 = -\nu \mathcal{S}_\alpha (g_1 - g_2) \quad (10e)$$

$$\partial_t \alpha_2 = -\nu \mathcal{S}_\alpha (g_2 - g_1) \quad (10f)$$

See Pelanti (IJMF 2022) for explicit expression of terms: \mathcal{S}_α , \mathcal{S}_p , \mathcal{S}_T

With initial condition Δg^0 , we find the **exact** solution of Δg over Δt :

$$\Delta g^* = \Delta g^0 \exp \{ -\nu (K_1 - K_2) \Delta t \}, \quad K_j = \frac{\mathcal{S}_p}{\rho_j} - s_j \mathcal{S}_T$$

As before, we may use exponential solution Δg to compute $\alpha_k \rho_k$ & α_k , $k = 1, 2$ under **stability condition** $K_1 - K_2 \geq 0$

Choice of relaxation parameters ?

Homogeneous hyperbolic step: remark

To achieve high resolution in step 1, care must be taken

- Positivity preserving

The larger phase N is, the more difficulty in obtaining positivity preserving is

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- Solution reconstruction
 - Physics-informed THINC (tangent of hyperbola for interface capturing) for interface sharpening in $N > 2$ is open
 - BVD (boundary variation diminishing); use 2 or more solution reconstruction techniques as basis, & take one by BVD criterion

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 - BVD (boundary variation diminishing); use 2 or more solution reconstruction techniques as basis, & take one by BVD criterion
- Riemann solver in finite-volume Godunov method

Solution differs not much by any state-of-the-art solver

Thank you