



# High fidelity anisotropic adaptive FEM: towards physical couplings occurring in turbulent boiling

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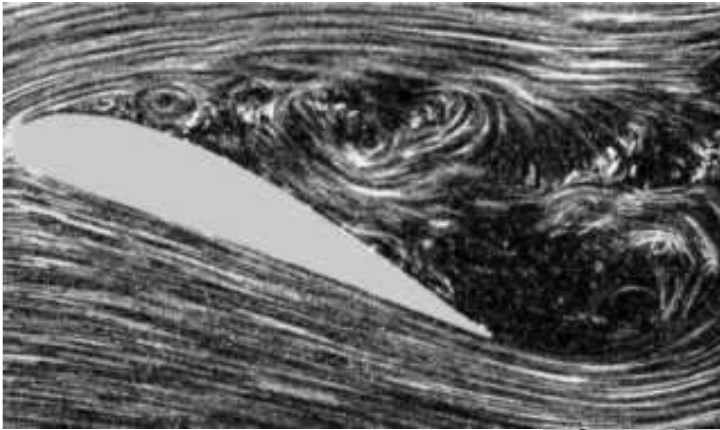
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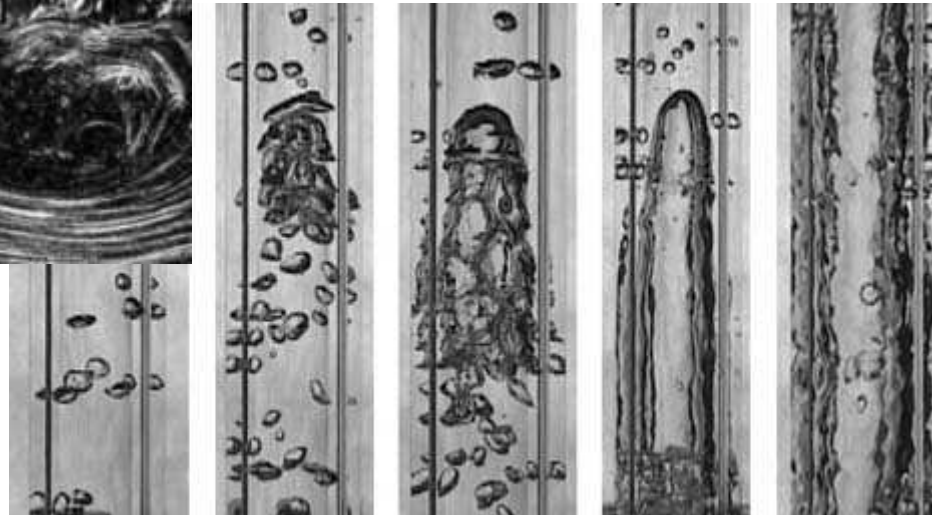
[elie.hachem@mines-paristech.fr](mailto:elie.hachem@mines-paristech.fr)

## Context:

→ Looking for a robust Eulerian multiphase framework



**gas-solid flows**



**liquid-gas flows**



**liquid-gaz-solid flows**

## Context:

→ Industrial application: **“Water Quench & Temper”**



- Multiphase flows
- Turbulent boiling
- Phase change
- Liquid-gaz-solid flows
- Water “agitators”
- Surface tension
- High thermal gradients
- ...

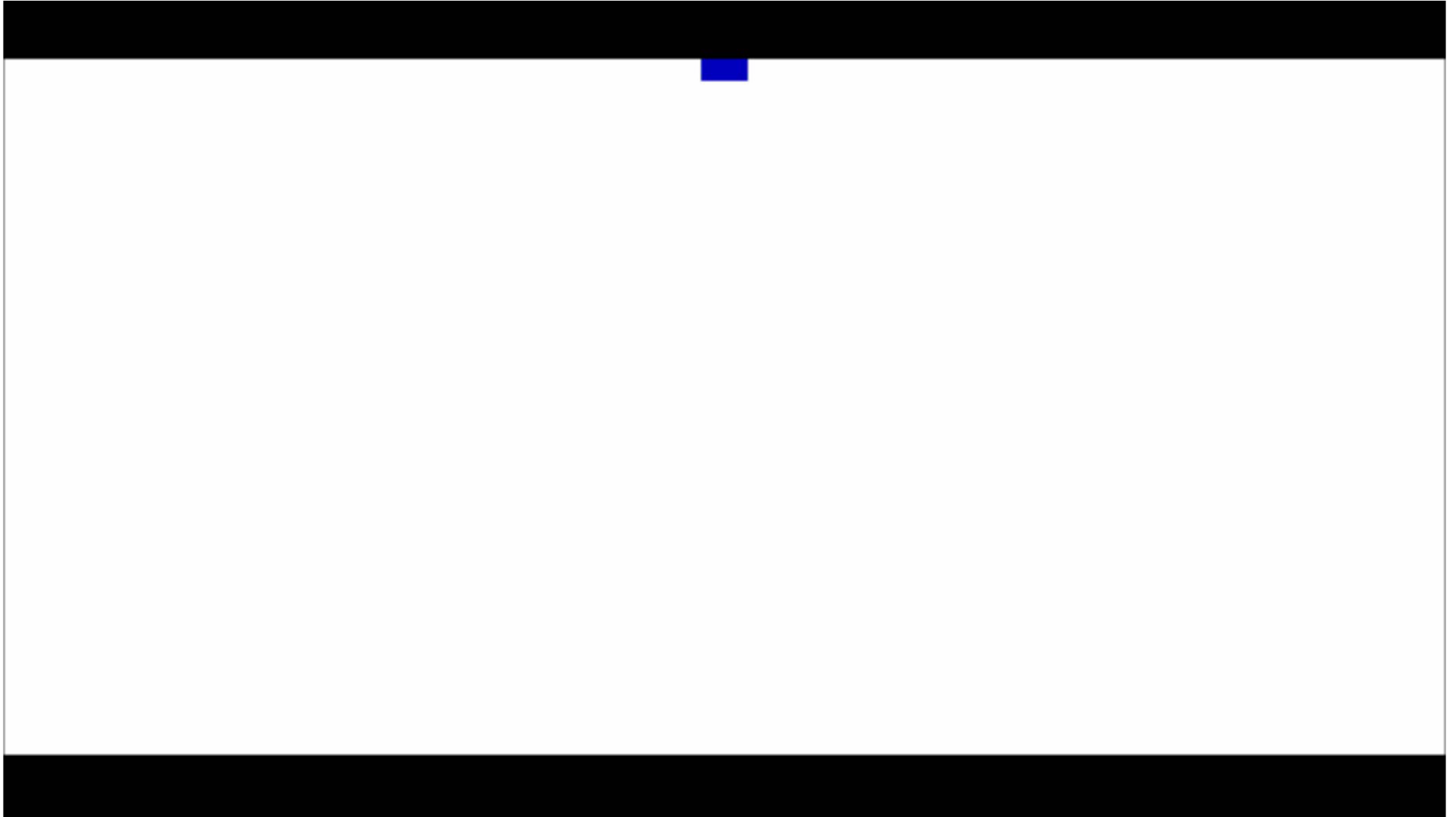
# Outline

## □ Eulerian multiphase framework

- FEM solver using Variational Multiscale Method
  - A conservative Level-set method
  - Implicit treatment of the surface tension
  - Anisotropic mesh adaptation
  - Extension towards a unified compressible-incompressible solver
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- Heat transfer and phase change
  - 2D and 3D validations

# High fidelity multiphase framework: illustration

Unsteady NS, Anisotropic mesh adaptation, regularisation, parallel computing



## ■ ■ FEM Flow solver:

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The strong form of the incompressible Navier Stokes equations reads:

$$\begin{cases} \rho(\delta_t \mathbf{v} + \mathbf{v} \cdot \nabla \mathbf{v}) - \nabla \cdot \boldsymbol{\sigma} = \mathbf{f} & \text{in } \Omega \times [0, T] \\ \nabla \cdot \mathbf{v} = 0 & \text{in } \Omega \times [0, T] \end{cases}$$

where  $\rho$  is the density,  $\eta$  is the viscosity, and the Cauchy stress tensor for a Newtonian fluid is given by:

$$\boldsymbol{\sigma} = 2\eta \boldsymbol{\varepsilon}(\mathbf{v}) - p \mathbf{I}_d$$

[A. Masud, R.A. Khurram, 2006]

[T.J.R. Hugues et al., 1998]

[V. Gravemeier, W.A. Wall, E. Ramm, 2004]

[L.P. Franca, A. Nesliturk, 2001]

[R. Codina, 2002]

The Galerkin discrete problem consists therefore in solving the following mixed problem:

Find a pair  $\mathbf{v}_h : [0, T] \rightarrow V_h$  and  $p_h : (0, T] \rightarrow P_h$ , such that:  $\forall (\mathbf{w}_h, q_h) \in V_{h,0} \times P_h$

$$\begin{cases} (\rho \delta_t \mathbf{v}_h, \mathbf{w}_h)_\Omega + (\rho \mathbf{v}_h \cdot \nabla \mathbf{v}_h, \mathbf{w}_h)_\Omega \\ \quad + (2\eta \boldsymbol{\varepsilon}(\mathbf{v}_h) : \boldsymbol{\varepsilon}(\mathbf{w}_h))_\Omega - (p_h, \nabla \cdot \mathbf{w}_h)_\Omega = (\mathbf{f}, \mathbf{w}_h)_\Omega \\ (\nabla \cdot \mathbf{v}_h, q_h)_\Omega = 0 \end{cases}$$

...the stability of this formulation depends on appropriate compatibility restrictions on the choice of the finite element spaces

...oscillations due to convection dominated flows

## ■ ■ Flow solver:

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VMS: Variational MultiScale

- VMS methods consider large scales which are defined by projection into appropriate spaces
- Models both velocity and pressure unresolved scales
- Similarity with the implicit version of LES
- Allows high density and viscosity ratios

Variational Multiscale formulation:  $\mathbf{v} = \mathbf{v}_h + \mathbf{v}' \quad p = p_h + p'$

- the use of equal order continuous interpolations
- preventing from oscillations due to convection dominated flows

find  $(\mathbf{v}_h + \mathbf{v}', p_h + p') \in V_h \oplus V' \times P_h \oplus P'$  such that

$$\begin{aligned}
 (\rho \delta_t(\mathbf{v}_h + \mathbf{v}'), \mathbf{w}_h + \mathbf{w}') + (\rho(\mathbf{v}_h + \mathbf{v}') \cdot \nabla(\mathbf{v}_h + \mathbf{v}'), \mathbf{w}_h + \mathbf{w}') - (p_h + p', \nabla \cdot (\mathbf{w}_h + \mathbf{w}')) \\
 + 2(\eta \varepsilon(\mathbf{v}_h + \mathbf{v}'), \varepsilon(\mathbf{w}_h + \mathbf{w}')) = \langle \mathbf{f}, \mathbf{w}_h + \mathbf{w}' \rangle \\
 (q_h + q', \nabla \cdot (\mathbf{v}_h + \mathbf{v}')) = 0
 \end{aligned}$$

for all  $(\mathbf{w}_h + \mathbf{w}', q_h + q') \in V_{h,0} \oplus V'_0 \times P_{h,0} \oplus P'_0$ .

## ■ ■ Flow solver:

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The implemented version:

- Static subscales
- Approximation of the nonlinear term using only the large-scale part
- Well adapted to anisotropic mesh adaptation

The subscales are approximated within each element K by:

$$\mathbf{v}' = \alpha_v \Pi'_v(\mathcal{R}_v), \quad p' = \alpha_p \Pi'_p(\mathcal{R}_p),$$

Where  $\mathcal{R}_c$  and  $\mathcal{R}_p$  are the finite element residuals:

$$\mathcal{R}_v = \mathbf{f} - \rho \delta_t \mathbf{v}_h - \rho \mathbf{v}_h \cdot \nabla \mathbf{v}_h - \nabla p_h + \nabla \cdot (2\eta \varepsilon(\mathbf{v}_h))$$

$$\mathcal{R}_p = -\nabla \cdot \mathbf{v}_h$$



## ■ ■ Flow solver:

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Variational MultiScale method:

- approximate the fine scale within each element  $K$
- inserting the expressions of the subscales in the coarse scale equations
- fully implicit resolution

$$\begin{aligned}
 & \frac{(\rho \delta_t \mathbf{v}_h, \mathbf{w}_h) + (\rho \mathbf{v}_h \cdot \nabla \mathbf{v}_h, \mathbf{w}_h) - (p_h, \nabla \cdot \mathbf{w}_h) + 2(\eta \varepsilon(\mathbf{v}_h), \varepsilon(\mathbf{w}_h))}{\phantom{K}} \\
 & + \sum_K \alpha_v (\rho \delta_t \mathbf{v}_h + \rho \mathbf{v}_h \cdot \nabla \mathbf{v}_h + \nabla p_h - \nabla \cdot (2\eta \varepsilon(\mathbf{v}_h)), \rho \mathbf{v}_h \cdot \nabla \mathbf{w}_h + \nabla \cdot (2\eta \varepsilon(\mathbf{w}_h)))_K \\
 & + \sum_K \alpha_p (\nabla \cdot \mathbf{v}_h, \nabla \cdot \mathbf{w}_h) \\
 & = \underline{\langle \mathbf{f}, \mathbf{w}_h \rangle} + \sum_K \alpha_v (\mathbf{f}, \rho \mathbf{v}_h \cdot \nabla \mathbf{w}_h + 2\eta \nabla \cdot \varepsilon(\mathbf{w}_h))_K \\
 & \underline{(q_h, \nabla \cdot \mathbf{v}_h)} + \sum_K \alpha_v (\rho \delta_t \mathbf{v}_h + \rho \mathbf{v}_h \cdot \nabla \mathbf{v}_h + \nabla p_h - \nabla \cdot (2\eta \varepsilon(\mathbf{v}_h)), \nabla q_h)_K \\
 & = \sum_K \alpha_v (\mathbf{f}, \nabla q_h)_K
 \end{aligned}$$

and the stabilization parameters:

$$\alpha_v = \left[ \left( \frac{c_1 \eta}{\rho h^2} \right)^2 + \left( \frac{c_2 \|\mathbf{v}_h\|_K}{h} \right)^2 \right]^{-1/2} \quad \alpha_p = \left[ \left( \frac{\eta}{\rho} \right)^2 + \left( \frac{c_2 \|\mathbf{v}_h\|_K h}{c_1} \right)^2 \right]^{1/2}$$

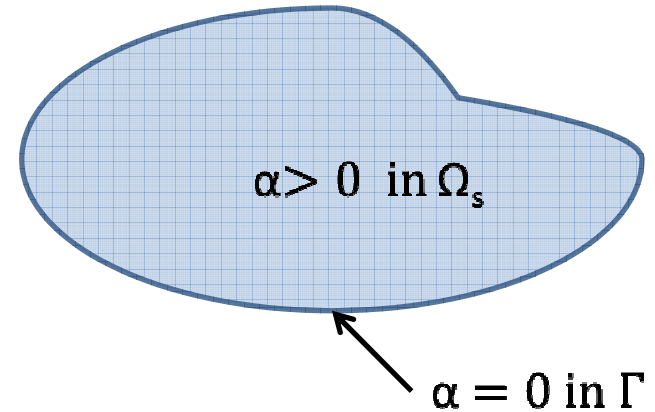
# 2-Level set

Basic definition

$$\alpha(X) = \begin{cases} -\text{dist}(X, \Gamma) & \text{if } X \in \Omega_f \\ 0 & \text{if } X \in \Gamma \\ \text{dist}(X, \Gamma) & \text{if } X \in \Omega_s \end{cases}$$

$$\|\nabla \alpha\| = 1$$

Phase representation  $\alpha < 0$  in  $\Omega_f$



(1) Transport equation  $\frac{\partial \alpha}{\partial t} + u \cdot \nabla \alpha = 0$

(2) Hamilton-Jacobi problem  $\frac{\partial \alpha}{\partial \tau} + s(\alpha)(\|\nabla \alpha\| - 1) = 0$

Two possibilities:

Solving (1) and (2) separately

Fedkiw 2009, Osher 2000, Sussman 2005

Embedding (2) in (1) : auto reinitialisation

Ville et.al. 2011, Bonito et al 2015

# Conservative Level Set method:

**Conservative** Level set method:

(1) Filtering  $\phi(\alpha) = \frac{1}{2} \left( 1 + \tanh \left( \frac{\alpha}{2\varepsilon} \right) \right)$

(2) Convection  $\frac{\partial \phi}{\partial t} + u \cdot \nabla \phi = 0$

(3) Reinitialization

$$\frac{\partial \phi}{\partial \tau} + \nabla \cdot \left( \phi(1 - \phi)n - \varepsilon((\nabla \phi \cdot n)n) \right) = 0$$

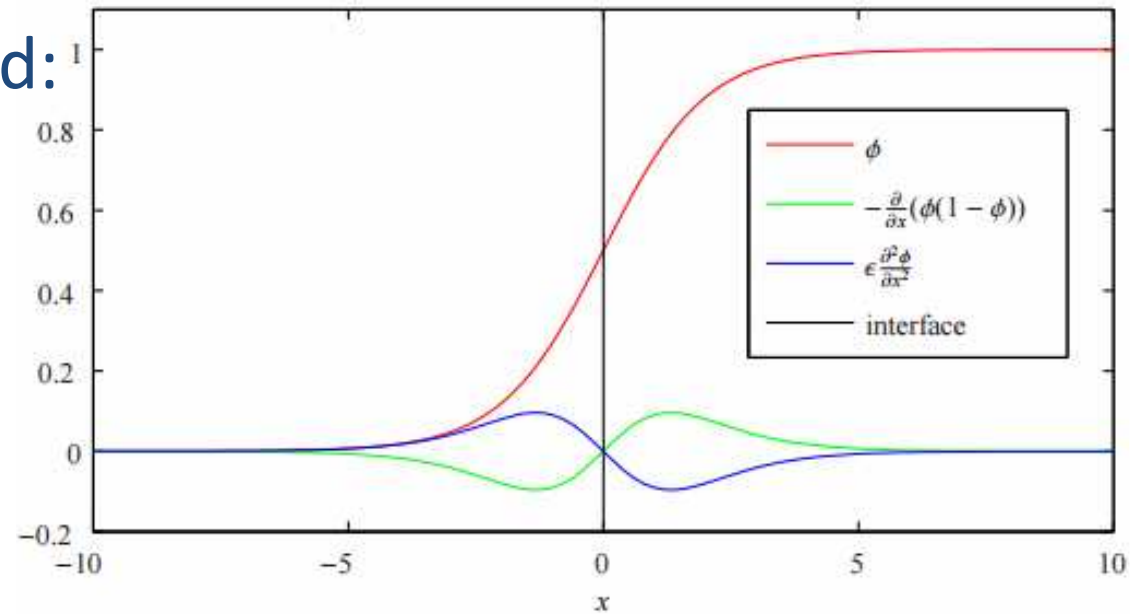
E. Olsson, G. Kreiss, A conservative level set method for two phase flow,  
*Journal of Computational Physics*, Volume 210, Issue 1, 2005, Pages 225-246

(2) + (3)  $\frac{\partial \phi}{\partial t} + u \cdot \nabla \phi = \nabla \cdot \left( \varepsilon(\nabla \phi \cdot n)n - \phi(1 - \phi)n \right)$

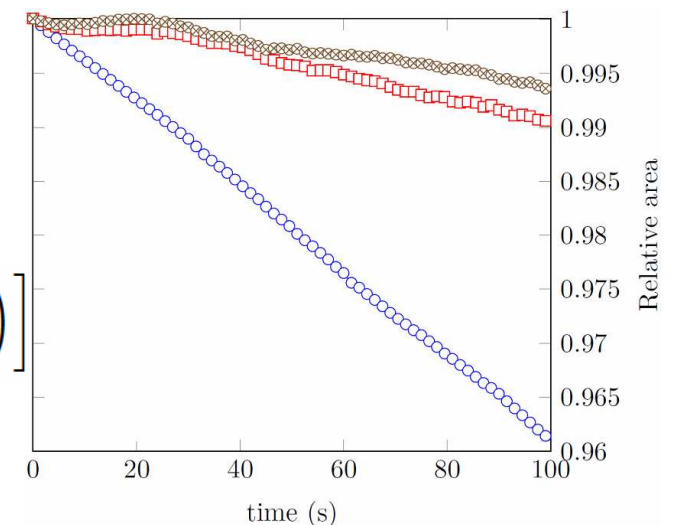


**Stabilized conservative FEM**  $\frac{\partial \phi}{\partial t} + u \cdot \nabla \phi = \nabla \cdot \left[ \chi \left( \varepsilon \nabla \phi - \phi(1 - \phi) \frac{\nabla \phi}{|\nabla \phi|} \right) \right]$

**X** : local Index



Walker, Müller 2014



### 3- Surface tension

Surface tension using CSF

$$f_{ST} = -\gamma\kappa\delta(\Gamma)\mathbf{n}$$

$$\mathbf{n} = \nabla\alpha/|\nabla\alpha| \quad \kappa = -\nabla\cdot\mathbf{n}$$

$\gamma$  is the surface tension coefficient

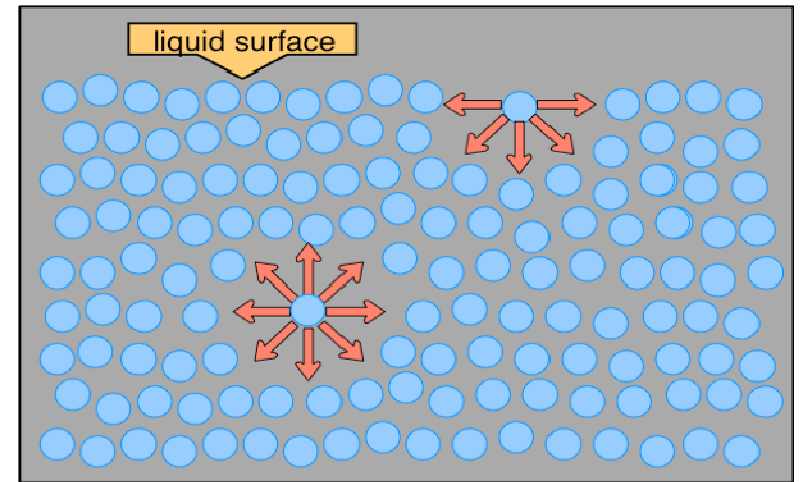
Usually implemented as a source term in NS equations

$$\begin{aligned} \rho(\partial_t u + u \cdot \nabla u) - \nabla \cdot (2\mu\varepsilon(u)) + \nabla p &= f + f_{ST} \\ \nabla \cdot u &= 0 \end{aligned}$$

Numerical analysis shows that: time-step restriction

$$\Delta t < (\Delta x)^{\frac{3}{2}} \sqrt{\frac{\bar{\rho}}{2\pi\gamma}}$$

Mesh adaptation:  $h \rightarrow 0$  so the restriction becomes stronger !!!



<http://butane.chem.uiuc.edu/>

### 3- Surface tension

Going back to the theorem of differential geometry

$$\Delta_s I_\Gamma = \nabla_s \cdot \nabla_s I_\Gamma = -\kappa \mathbf{n}$$

Implicit time integration of the interface position

$$I_\Gamma^{n+1} = I_\Gamma^n + \mathbf{u}^{n+1} \Delta t$$

Applying the theorem to the interface position

$$\begin{aligned} \Delta_s I_\Gamma^{n+1} &= \Delta_s I_\Gamma^n + \Delta t \Delta_s \mathbf{u}^{n+1} \\ -(\kappa \mathbf{n})^{n+1} &= -(\kappa \mathbf{n})^n + \Delta t (\Delta_s \mathbf{u}^{n+1}) \\ -\gamma (\kappa \mathbf{n})^{n+1} &= -\gamma \kappa \mathbf{n} + \gamma \Delta t (\Delta_s \mathbf{u}^{n+1}) \end{aligned}$$

Decomposition of the surface Laplacian into a standard Laplacian

$$\Delta_s = \nabla_s^2 = \nabla^2 - \frac{\partial^2}{\partial \mathbf{n}^2} - \kappa \frac{\partial}{\partial \mathbf{n}} \quad \text{with} \quad \frac{\partial \mathbf{u}}{\partial \mathbf{n}} = \nabla \mathbf{u} \cdot \mathbf{n}$$

Semi-implicit surface tension

$$f_{\text{ST}} = \boxed{-\gamma \kappa \delta(\alpha) \mathbf{n}} - \gamma \delta(\alpha) \Delta t \left( \frac{\partial^2 \mathbf{u}}{\partial \mathbf{n}^2} + \kappa \frac{\partial \mathbf{u}}{\partial \mathbf{n}} - \nabla^2 \mathbf{u}^{n+1} \right)$$

### 3- Modifying NS equations

$$f_{ST} = -\gamma\kappa\delta(\alpha)n - \gamma\delta(\alpha)\Delta t \left( \frac{\partial^2 u}{\partial n^2} + \kappa \frac{\partial u}{\partial n} - \nabla^2 u^{n+1} \right)$$

#### Variational formulation

$$\begin{aligned} \blacksquare \quad & \rho(\partial_t u_h, v_h)_\Omega + \rho(u_h^i \cdot \nabla u_h, v_h)_\Omega - \sum_{K \in \mathcal{T}_h} (\tau_K \mathcal{R}_M, \rho u_h \nabla v_h)_K + (2\mu \varepsilon(u_h) : \varepsilon(v_h))_\Omega \\ & - (p_h, \nabla \cdot v_h)_\Omega + \gamma\delta(\alpha)\Delta t (\nabla u_h : \nabla v_h)_\Omega + \sum_{K \in \mathcal{T}_h} (\tau_C \mathcal{R}_C, \nabla \cdot v_h)_K = \\ & (f - \boxed{\gamma\delta(\alpha)\kappa n} - \gamma\delta(\alpha)\Delta t (\partial_{nn} u_h^i + \kappa \partial_n u_h^i), v_h)_\Omega \\ \blacksquare \quad & (\nabla u_h, q_h)_\Omega - \sum_{K \in \mathcal{T}_h} (\tau_K \mathcal{R}_M, \nabla q_h)_K = 0 \end{aligned}$$

#### Residuals

$$\begin{aligned} \mathcal{R}_M &= f - \boxed{\gamma\delta(\alpha)\kappa n} - \gamma\delta(\alpha)\Delta t (\partial_{nn} u_h^i + \kappa \partial_n u_h^i) - \rho \partial_t u_h - \rho u_h^i \cdot \nabla u_h - \nabla p_h \\ \mathcal{R}_C &= -\nabla \cdot u_h \end{aligned}$$

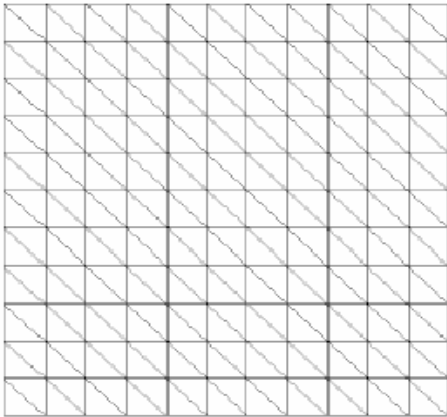
## ■ ■ 4- Anisotropic mesh adaptation

We are concern to capture automatically:

(i) boundary layers

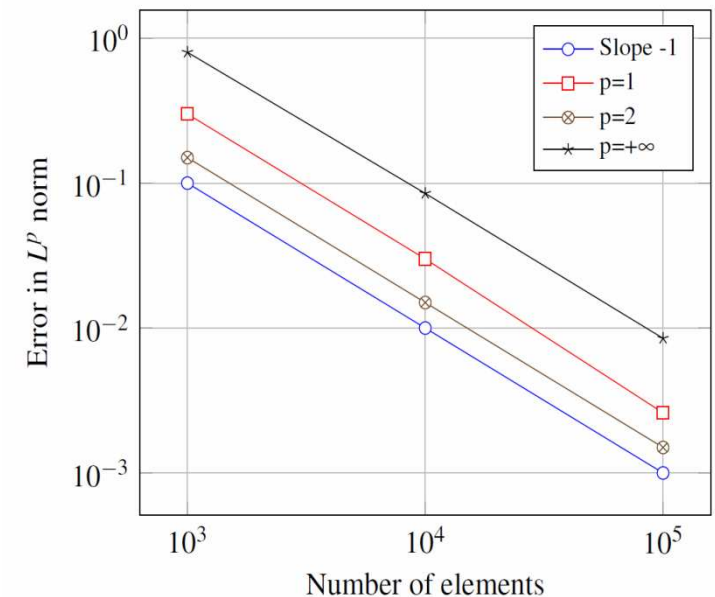
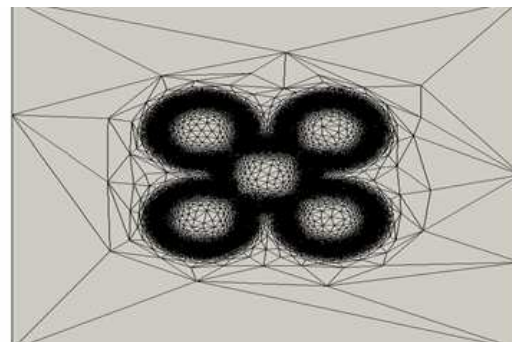
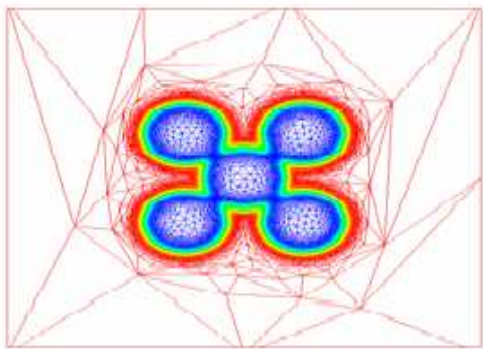
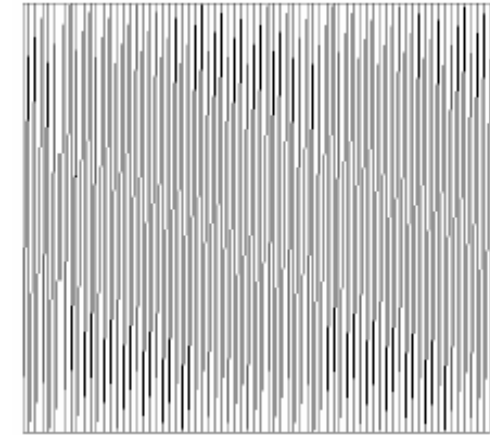
(ii) inner layers

(iii) flow detachments



$$+ M = \begin{pmatrix} \frac{1}{0.01^2} & \\ & \frac{1}{1^2} \end{pmatrix} + \text{imrpoved remesher} =$$

Metric (directions, size)

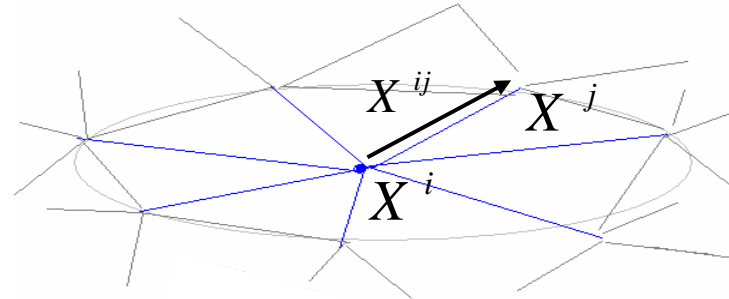




## ■ ■ 4- Anisotropic mesh adaptation

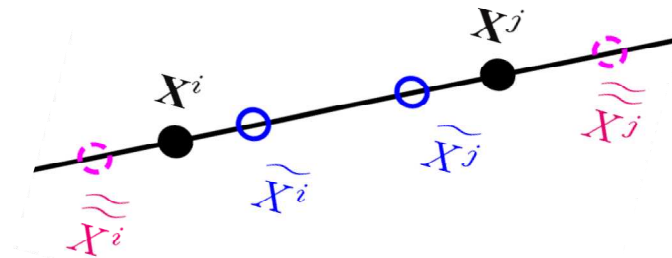
Candidate for directions:

$$\mathbb{X}^i = \frac{d}{|\Gamma(i)|} \sum_{j \in \Gamma(i)} \mathbf{X}^{ij} \otimes \mathbf{X}^{ij}$$



Control the size of each edge  $X^{ij}$  using a stretching factor:

$$\widetilde{\mathbf{X}}^{ij} = s_{ij} \mathbf{X}^{ij}$$



Drive these stretching factors using an edge based error estimator:

$$s_{ij} = \left( \frac{e}{e(N)} \right)^{-\frac{1}{2}} = \left( \frac{\sum_i n^i(1)}{N} \right)^{\frac{2}{d}} e_{ij}^{-1/2}$$

$$\widetilde{\mathbb{M}}^i = \frac{|\Gamma(i)|}{d} \left( \widetilde{\mathbb{X}}^i \right)^{-1}$$

T. Coupez and E. Hachem, Solution of High-Reynolds Incompressible Flow with Stabilized Finite Element and Adaptive Anisotropic Meshing, Computer Methods in Applied Mechanics and Engineering, Vol. 267, pp. 65-85, 2013

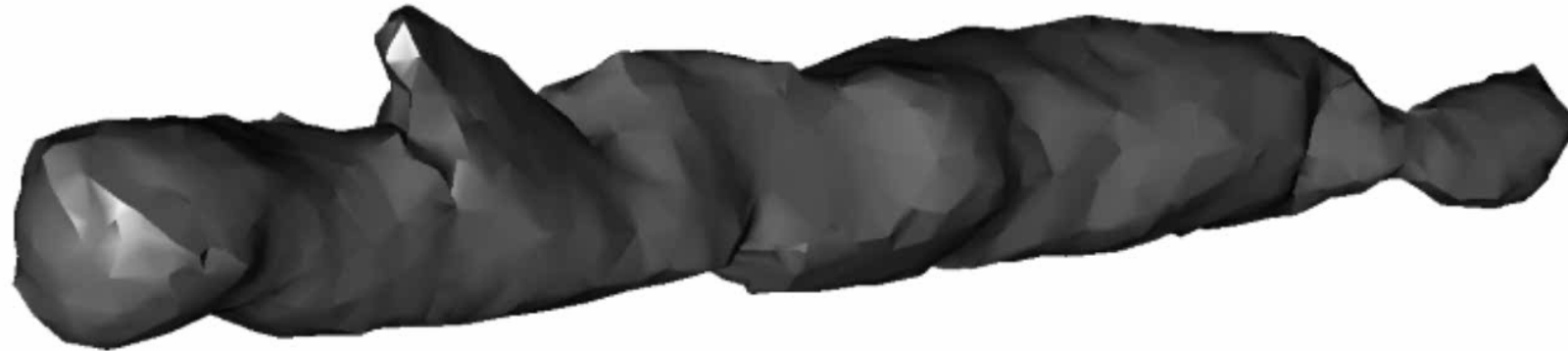
L. Billon, Y. Mesri, E. Hachem, Anisotropic boundary layer mesh generation for immersed complex geometries, Engineering with Computers, pp. 1-12, 2016



## Illustration 1: complex geometry

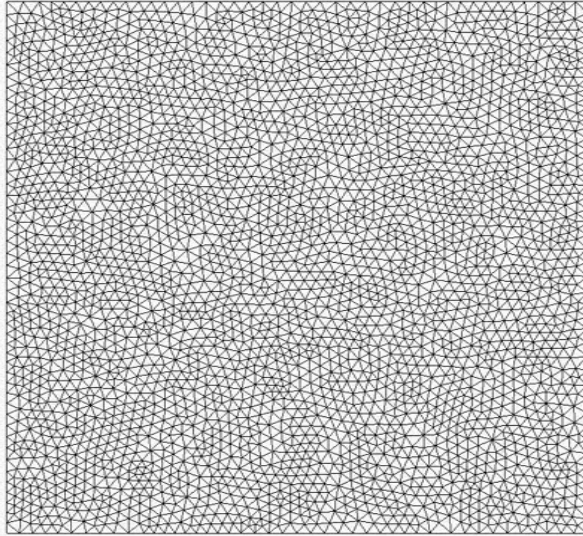
❑ Unlock new features in complex geometries

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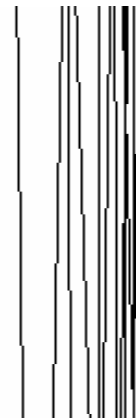
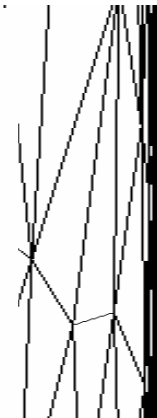
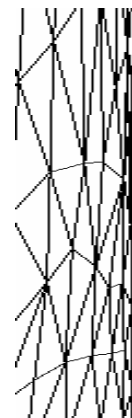
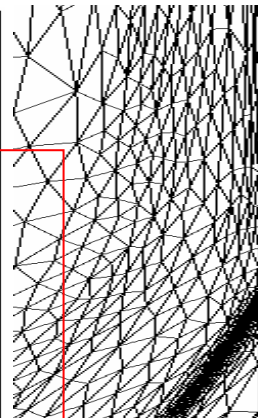
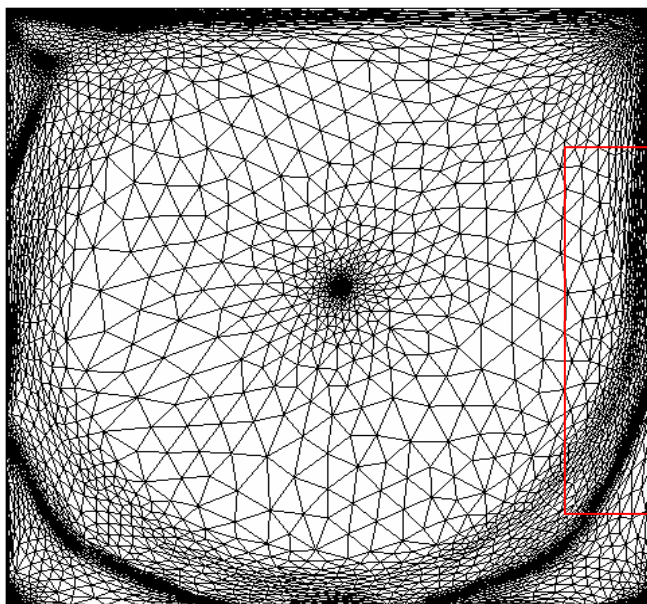
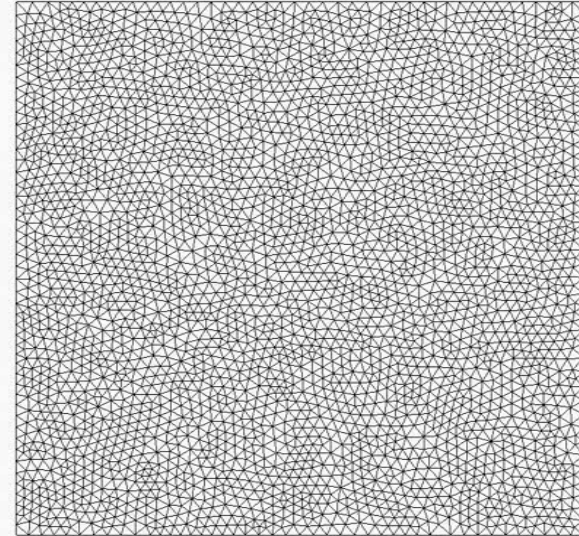


## ■ ■ Illustration 2: NS with dynamic anisotropic meshing

$Re = 20000$



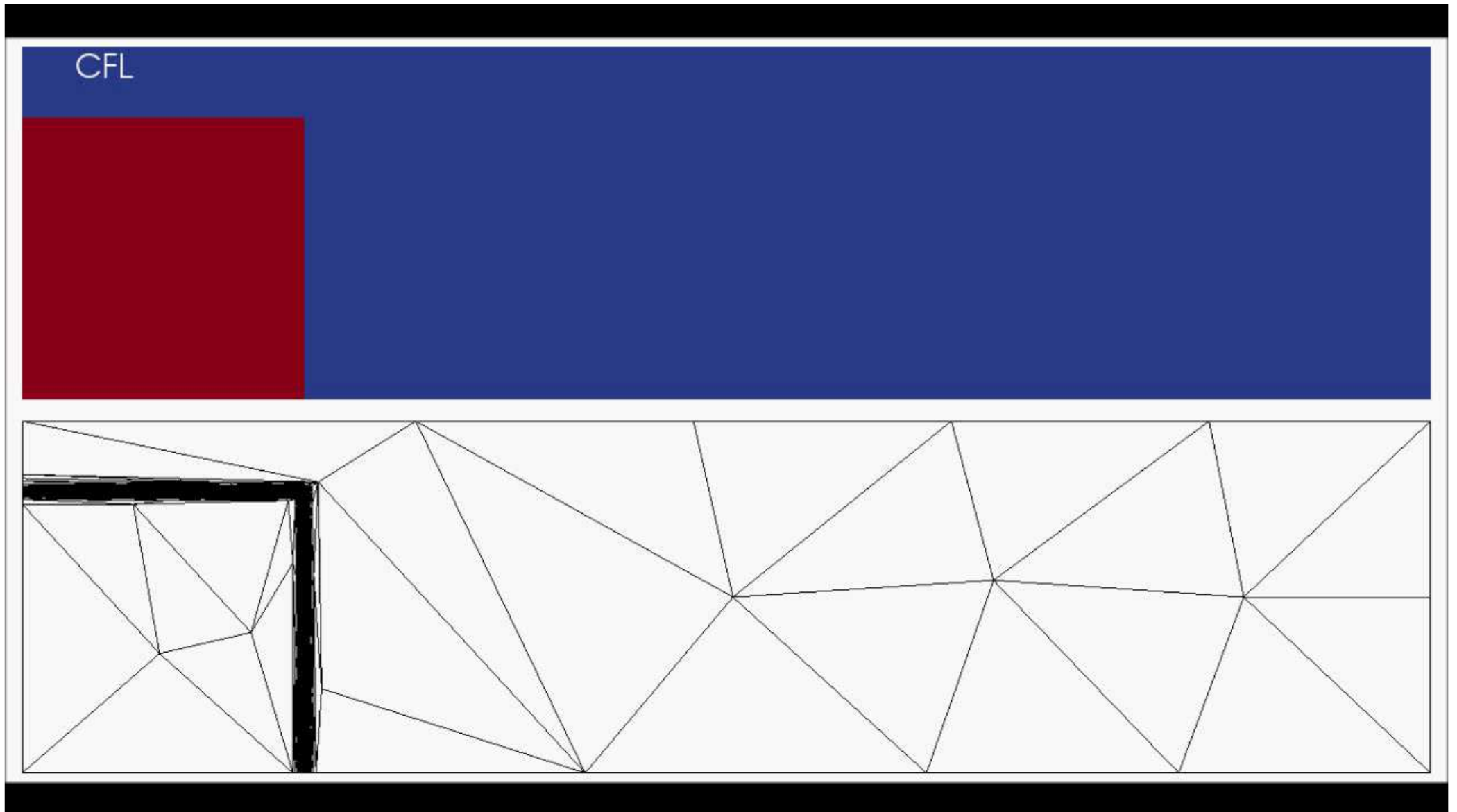
$Re = 100000$



J. L. Guermond and P. D. Mineev, Start-up flow in a three-dimensional lid-driven cavity by means of a massively parallel direction splitting algorithm *Int. J. Numer. Meth. Fluids* (2011)

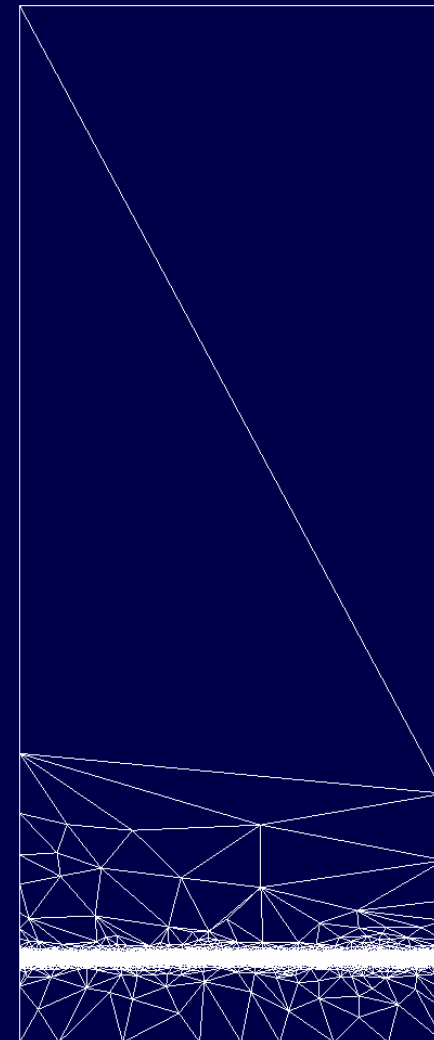
### Illustration 3: Dam breaking (water column with surface tension)

❑ Independent from the problem at hand



## Illustration 4: Filling and dome formation

- ❑ Length redistribution under the constraint of a fixed number of nodes



## 5- Unified Compressible/Incompressible solver

Navier-Stokes equations

$$\begin{aligned}\rho(\partial_t u + u \cdot \nabla u) - \nabla \cdot \sigma &= f \quad \text{in } \Omega \times [0, T] \\ \nabla \cdot u &= 0 \quad \text{in } \Omega \times [0, T]\end{aligned}$$

$$\frac{d\rho}{dt} = \left(\frac{\partial \rho}{\partial T}\right)_p \frac{dT}{dt} + \left(\frac{\partial \rho}{\partial p}\right)_T \frac{dp}{dt} \quad \longrightarrow \quad \chi_p = \frac{1}{\rho} \left(\frac{\partial \rho}{\partial p}\right)_T \quad \text{and} \quad \chi_T = \frac{1}{\rho} \left(\frac{\partial \rho}{\partial T}\right)_p$$

$\chi_T$  is the volume expansivity  
 $\chi_p$  is the isothermal compressibility coefficient

Conservation equation

$$\nabla \cdot u + \chi_p \frac{\partial p}{\partial t} + \chi_p u \cdot \nabla p = \chi_T \frac{dT}{dt}$$

M. Billaud, G. Gallice, B. Nkonga, A simple stabilized finite element method for solving two phase compressible–incompressible interface flows, *Computer Methods in Applied Mechanics and Engineering*, Volume 200, Issues 9–12, 2011, pp.1272-1290

## 5-Unified Compressible/Incompressible solver

$$\rho \frac{\partial u}{\partial t} + \rho u \cdot \nabla u - \nabla \cdot (2\mu \varepsilon(u)) + \nabla p = f_v$$

$$\nabla \cdot u + \chi_P \frac{\partial p}{\partial t} + \chi_P u \cdot \nabla p = f_p$$

By splitting the velocity and the pressure into a coarse scale and a fine scale:  
Variational Multiscale Stabilized Finite Element Method

$$\left( \frac{\rho \partial(u_h + \tilde{u})}{\partial t}, v_h \right) + (\rho(u_h + \tilde{u}) \cdot \nabla(u_h + \tilde{u}), v_h) - (p_h + \tilde{p}, \nabla \cdot v_h) + (2\eta \varepsilon(u_h) : \varepsilon(v_h)) = (f_v, v_h) \quad \forall v_h \in \mathcal{V}_h$$

$$(\nabla \cdot (u_h + \tilde{u}), q_h) + \chi_P \left( \frac{\partial(p_h + \tilde{p})}{\partial t}, q_h \right) + \chi_P ((u_h + \tilde{u}) \cdot \nabla(p_h + \tilde{p}), q_h) = (f_p, q_h) \quad \forall q_h \in \mathcal{Q}_h$$

$$\tilde{u} = \sum_{K \in \mathcal{S}_h} \tau_u \tilde{P}_u(R_u)$$

$$\tilde{p} = \sum_{K \in \mathcal{S}_h} \tau_c \tilde{P}_c(R_c)$$

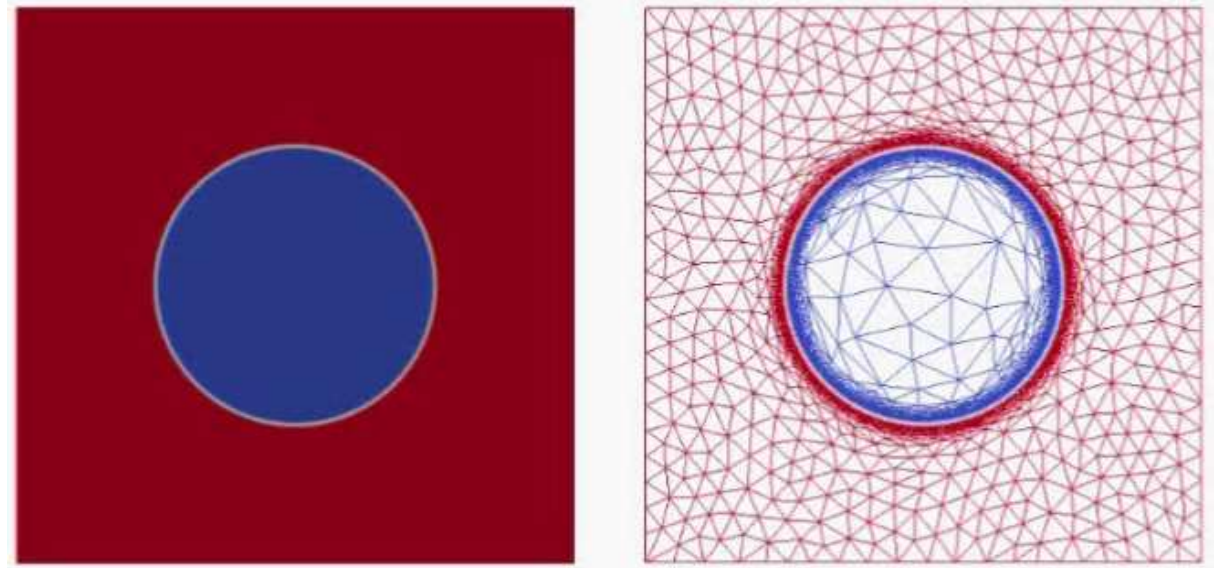
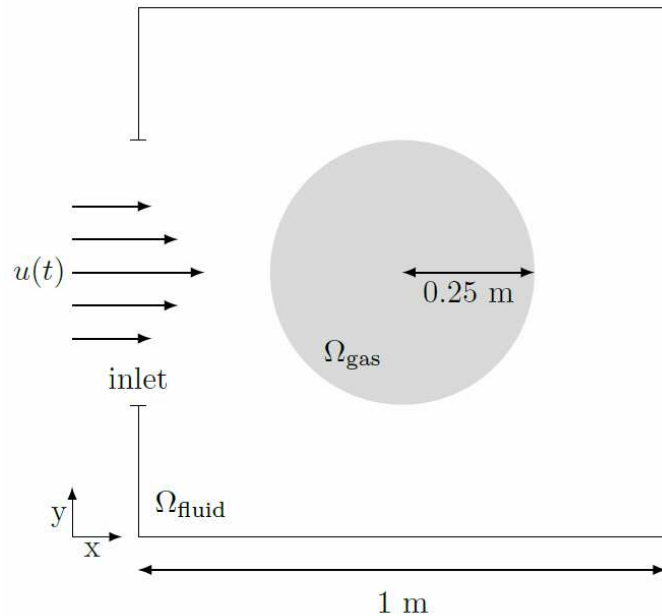
$$R_u = f_v - \rho \frac{\partial u_h}{\partial t} - \rho u_h^c \cdot \nabla u_h + \nabla \cdot (2\mu \varepsilon(u_h)) - \nabla p_h$$

$$R_c = \underline{\underline{f_p}} - \underline{\underline{\nabla \cdot u_h}} - \underline{\underline{\chi_P \frac{\partial p_h}{\partial t}}} - \underline{\underline{\chi_P u_h^c \cdot \nabla p_h}}$$

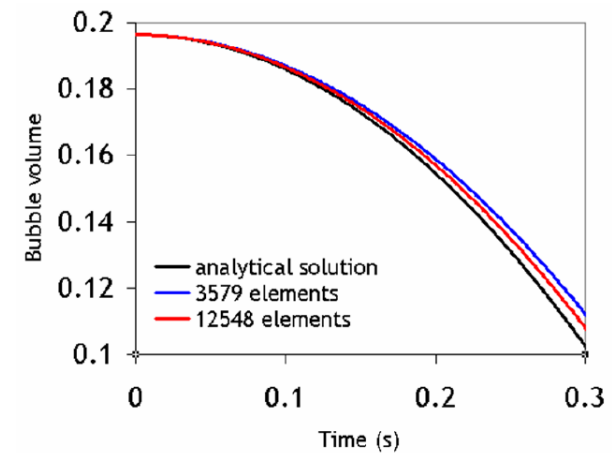


## 5-Unified Compressible/Incompressible solver

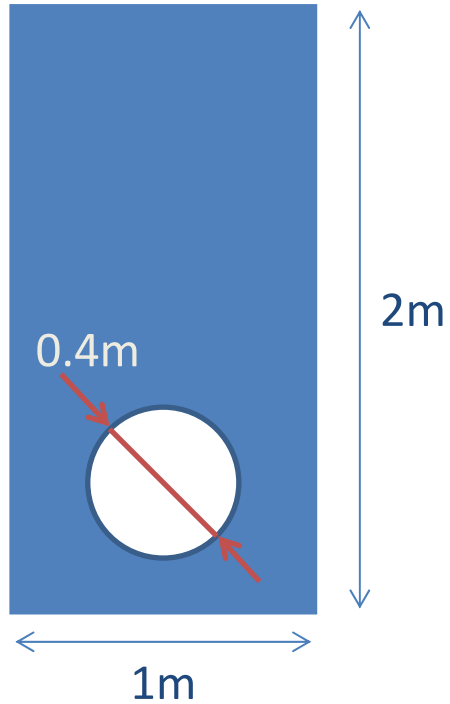
### Compression of a bubble – Challenging case



E. Hachem, M. Khalloufi, J. Bruchon, R. Valette, Y. Mesri, Unified adaptive Variational MultiScale method for two phase compressible-incompressible flows, Computer Methods in Applied Mechanics and Engineering, Vol. 308, pp. 238-255, 2016



## 2D and 3D validations



- Liquid  
Density:  $10^4 \text{ kg/m}^3$   
Viscosity:  $1 \text{ kg/(m.s)}$
- Vapor  
Density:  $10^3 \text{ kg/m}^3$   
Viscosity:  $1 \text{ kg/(m.s)}$

Surface tension  $0,5 \text{ kg/s}^2$   
Gravity  $g = -8 \times 10^{-4} \text{ m/s}^2$

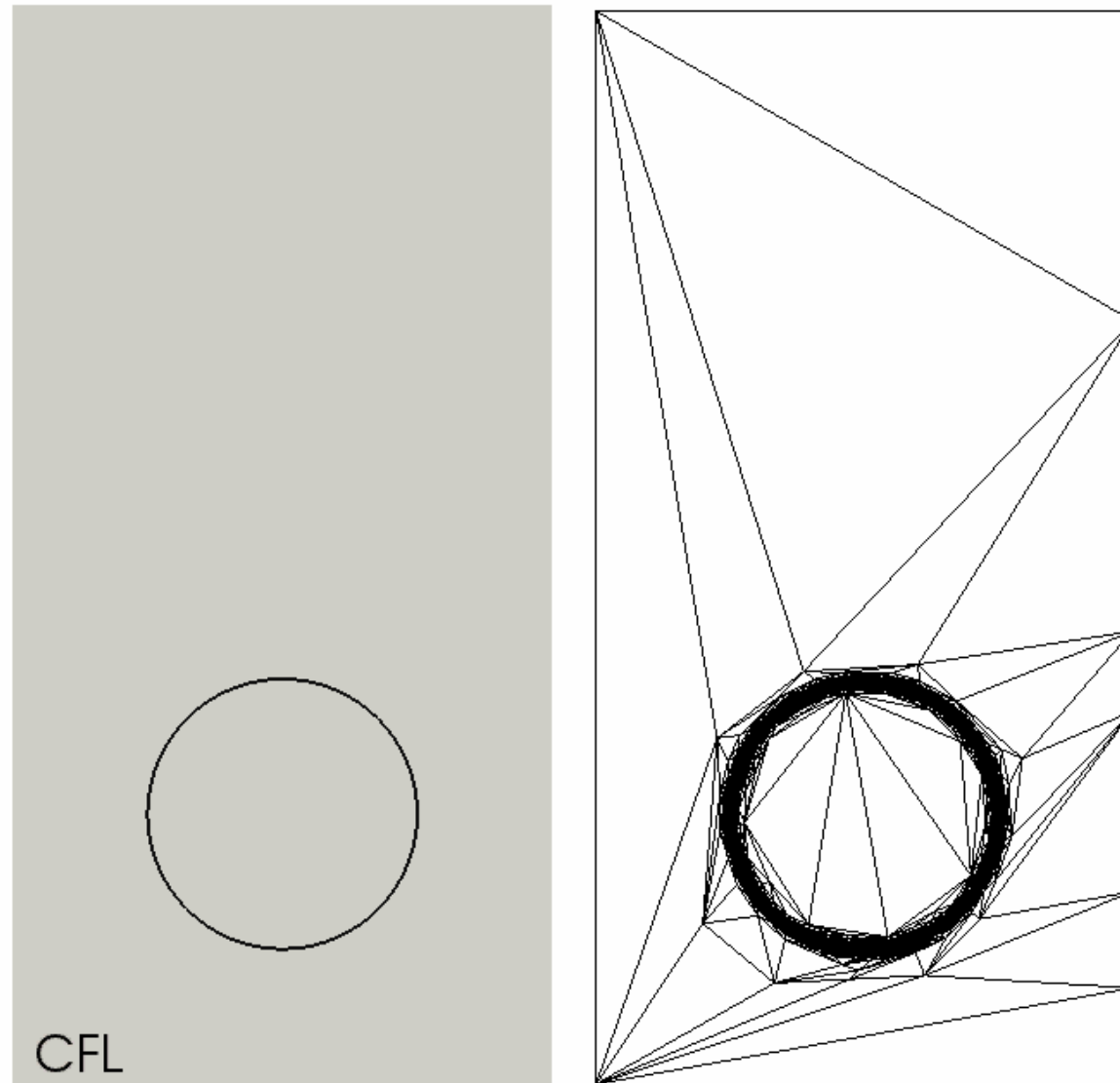
Mesh size  $h = 1/80$



# Validation: Rising bubble with mesh adaptation with / without surface tension



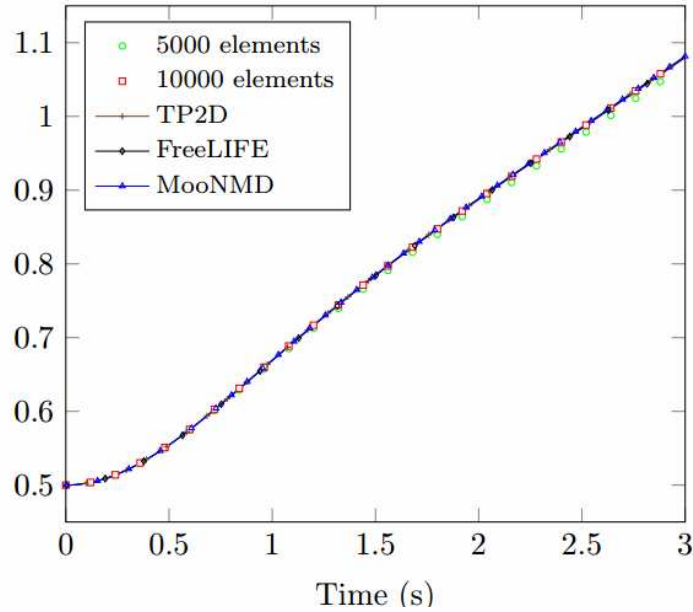
## Validation: Rising bubble with mesh adaptation



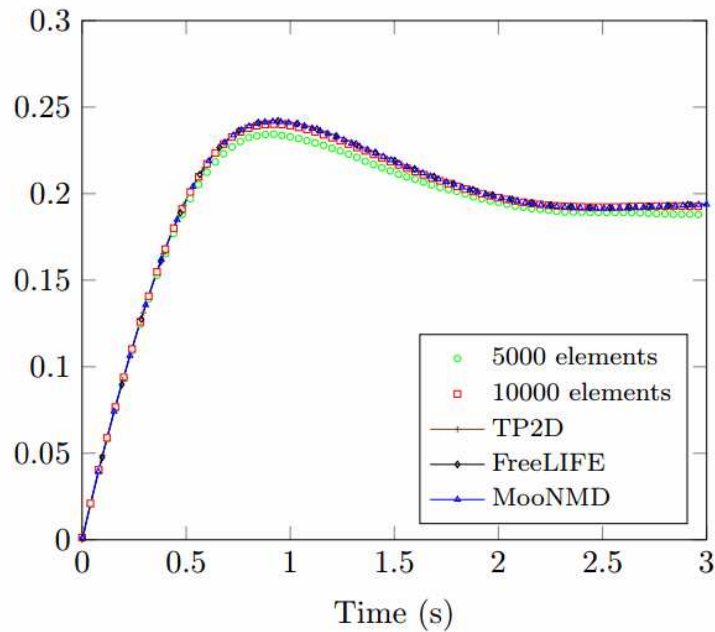
# Validation: Rising bubble with mesh adaptation

Case1

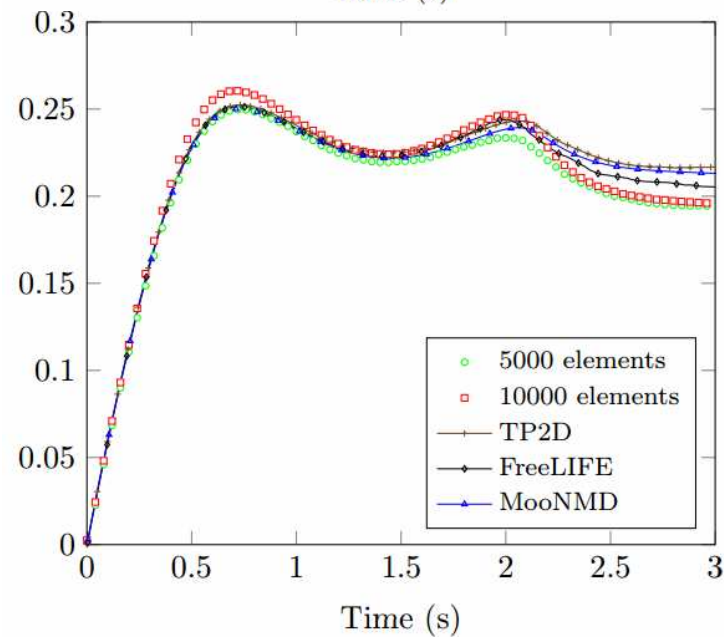
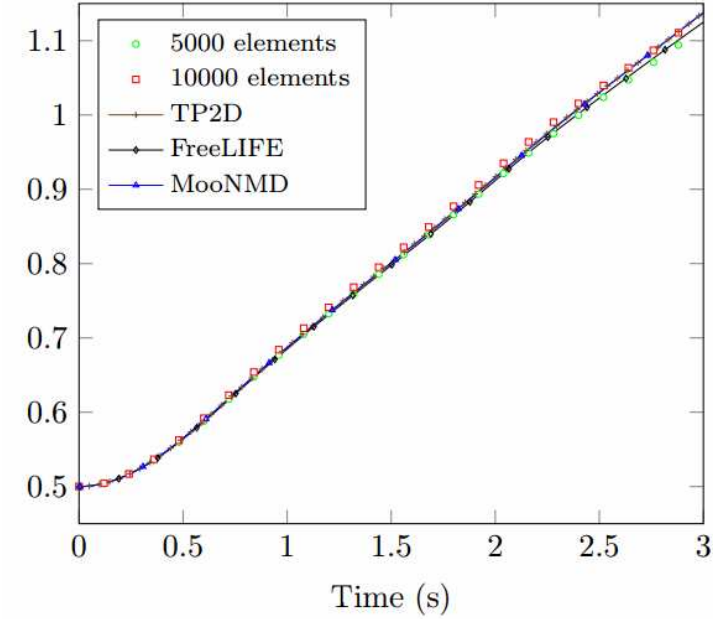
Position of the  
center of mass



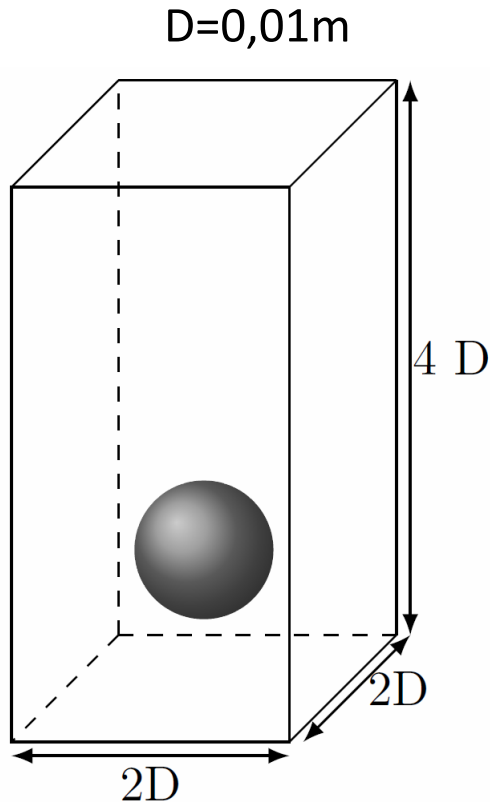
Rising velocity



Case2



## Validation: 3D Rising bubble with mesh adaptation

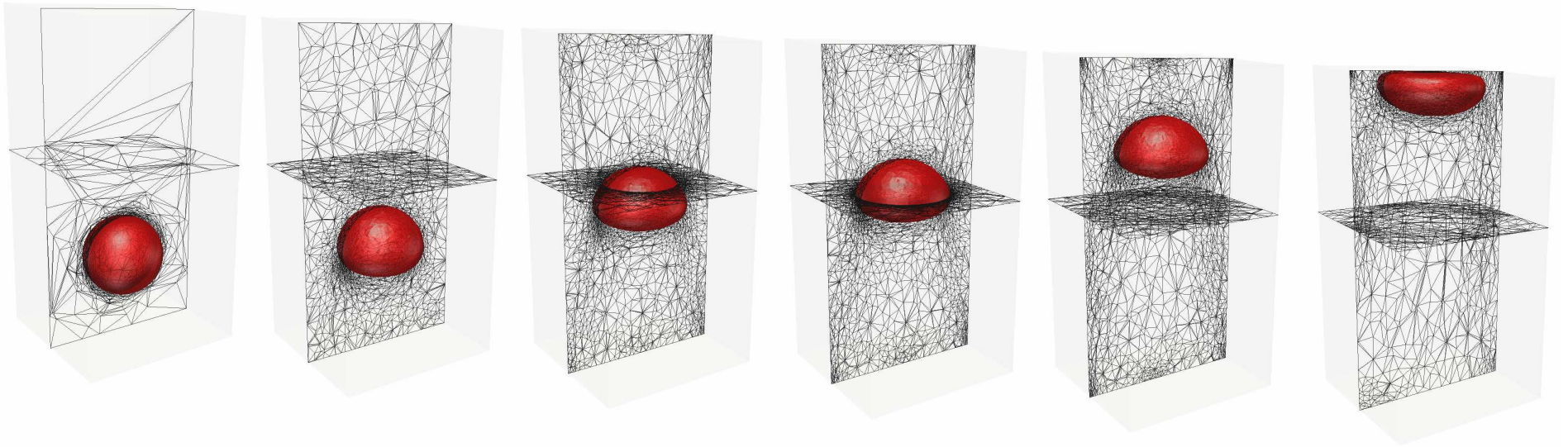


- Outer fluid  
Density  $1000 \text{ kg/m}^3$   
Viscosity  $0.35 \text{ kg/(m.s)}$
- Bubble  
Density  $1.225 \text{ kg/m}^3$   
Viscosity  $0.00358 \text{ kg/(m.s)}$

Surface tension  $0.11 \text{ kg/s}^2$   
Gravity  $g=9.81 \text{ m/s}^2$

U. Rasthofer, F. Henke, W.A. Wall, V. Gravemeier, An extended residual-based variational multiscale method for two-phase flow including surface tension, Computer Methods in Applied Mechanics and Engineering, Volume 200, Issues 21–22, 1 May 2011, Pages 1866-1876

## Validation: 3D Rising bubble with mesh adaptation



With surface tension

## 6- Heat transfer and Phase change

Energy conservation (neglecting viscosity and capillary forces)

$$\rho c_p \left( \frac{\partial T}{\partial t} + u \cdot \nabla T \right) - \nabla \cdot (k \nabla T) = - \left( L + (c_p^v - c_p^l)(T - T_{\text{vap}}) \right) \dot{m} \delta |\nabla \phi| \frac{\rho^2}{\rho_v \rho_l}$$

Mass conservation

$$\nabla \cdot u = \dot{m} \left( \frac{1}{\rho_v} - \frac{1}{\rho_l} \right) |\nabla \alpha| \delta$$

Interface evolution

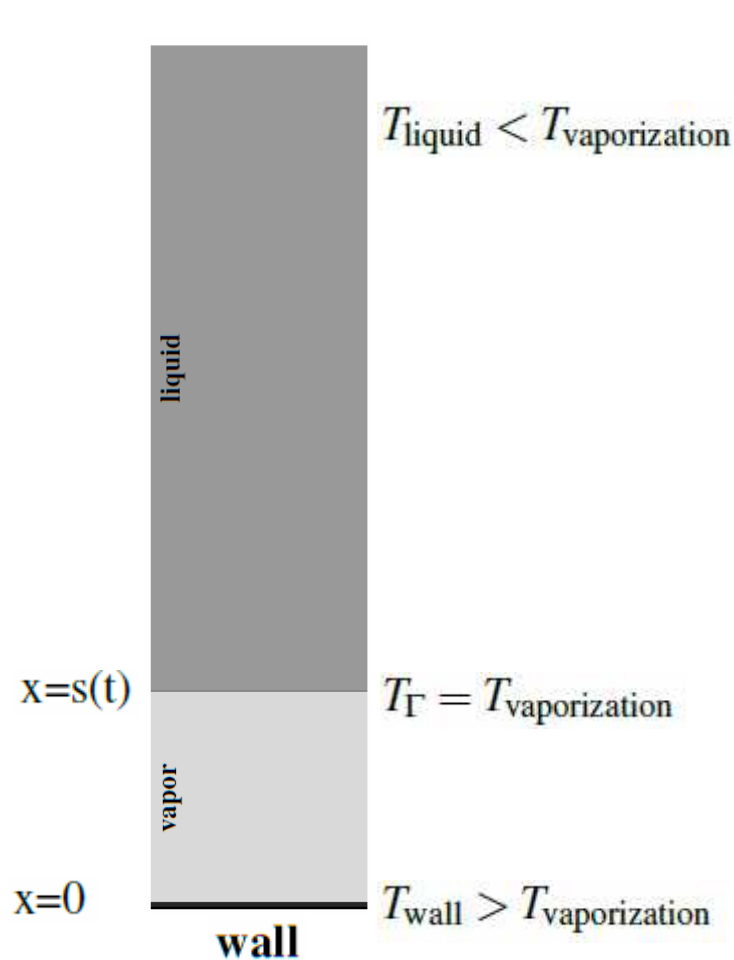
$$\frac{\partial \phi}{\partial t} + \left[ u - \frac{\rho}{\rho_l \rho_v} \dot{m} \frac{\nabla \phi}{|\nabla \phi|} \right] \cdot \nabla \phi = 0$$

Recall the density distribution

$$\rho = (\rho_v - \rho_l)H + \rho_l$$



## 6- Heat transfer and Phase change: Stefan problem



$$\rho c_p \frac{\partial T}{\partial t} - k \frac{\partial^2 T}{\partial x^2} = 0$$

$$T(x, t) = T_{\text{wall}} + \frac{T_{\text{vaporization}} - T_{\text{wall}}}{\text{erf}\left(\frac{s}{2\sqrt{\alpha_v t}}\right)} \text{erf}\left(\frac{x}{2\sqrt{\alpha_v t}}\right)$$

$$\text{erf}(x) = \frac{2}{\sqrt{\pi}} \int_0^x \exp(-t^2) dt$$

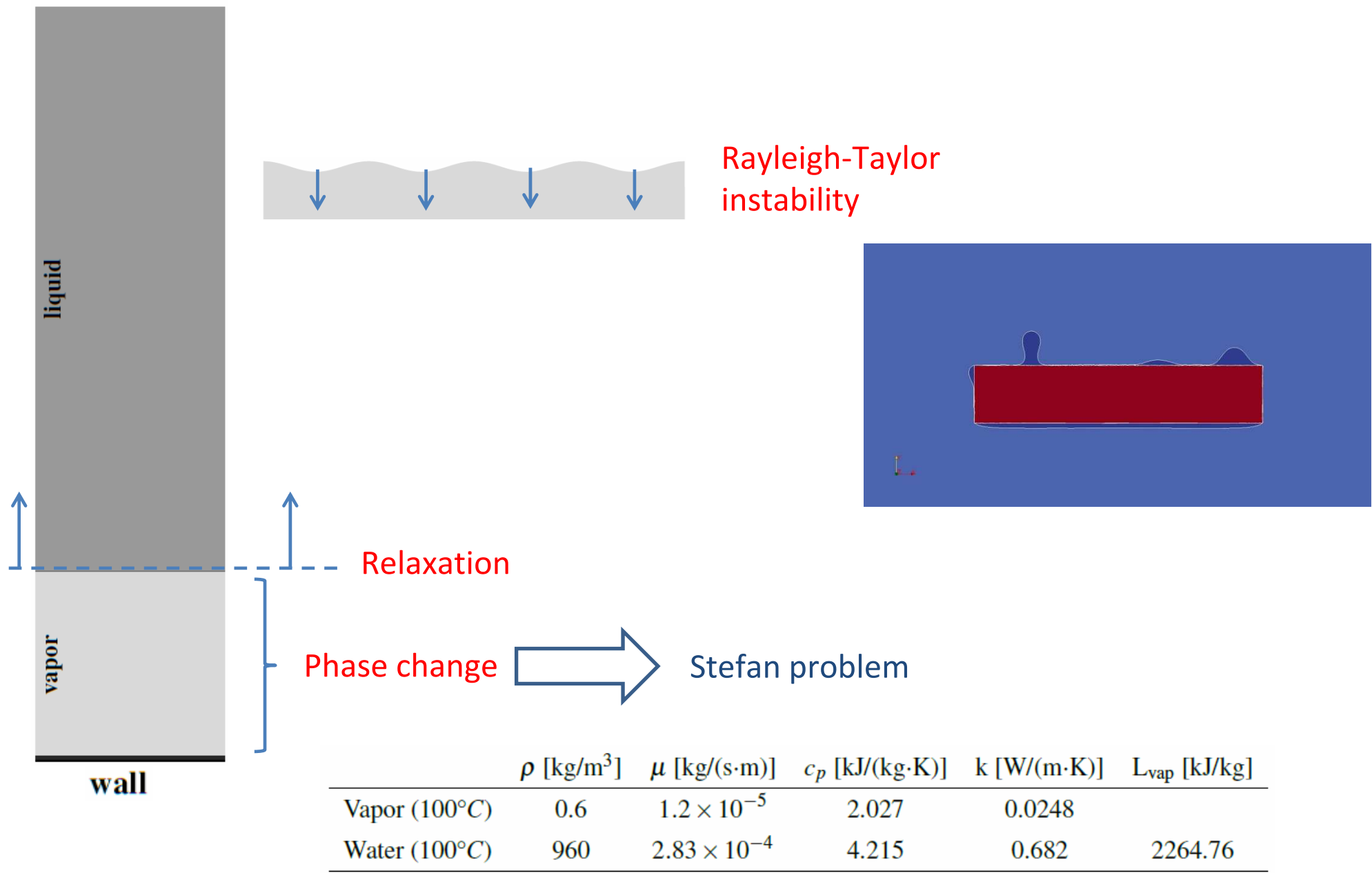
Stefan condition with constant density

$$\rho L \frac{ds}{dt} = (-k_v \nabla T_v + k_l \nabla T_l) \cdot \vec{e}_x$$

Stefan condition with variable density

$$-\rho_v L_{\text{vap}} \frac{ds}{dt} - \frac{1}{2} \rho_v \left(1 - \frac{\rho_v}{\rho_l}\right)^2 \left(\frac{ds}{dt}\right)^3 = (-k_l \nabla T_l + k_v \nabla T_v) \cdot \vec{e}_x$$

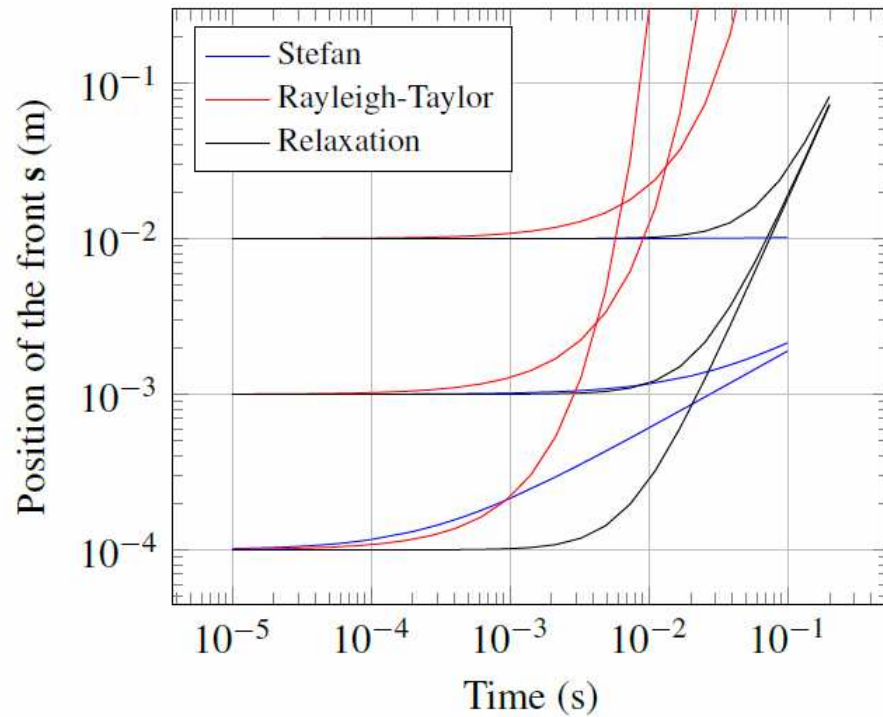
## 6- Heat transfer and Phase change: zoom



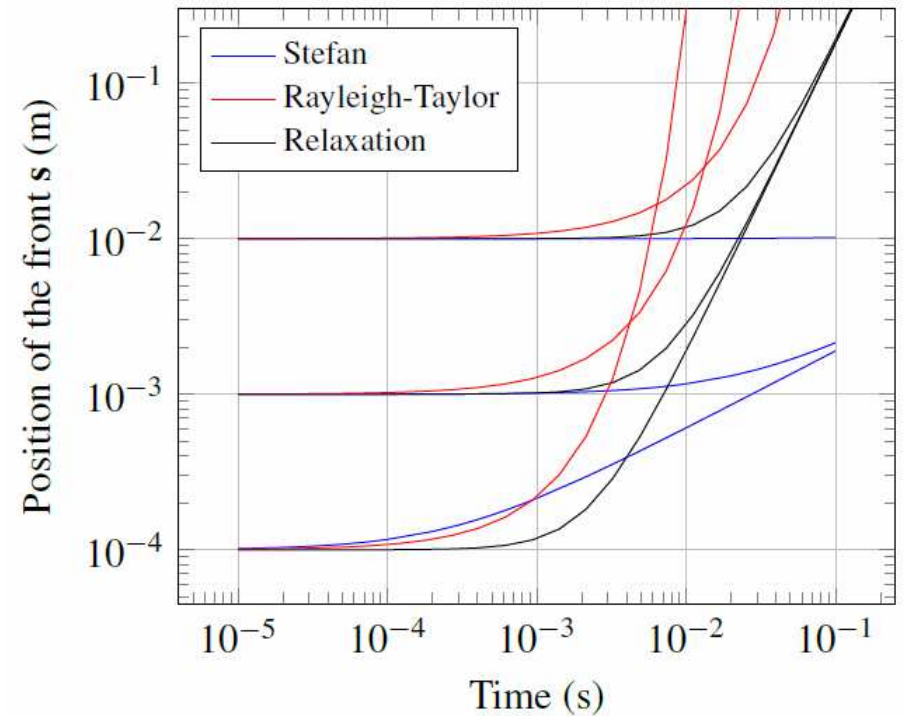


## 6- Heat transfer and Phase change:

For a given initial thickness of the film



Water level : 1m above the vapor  
film  $P=1.1$ bar

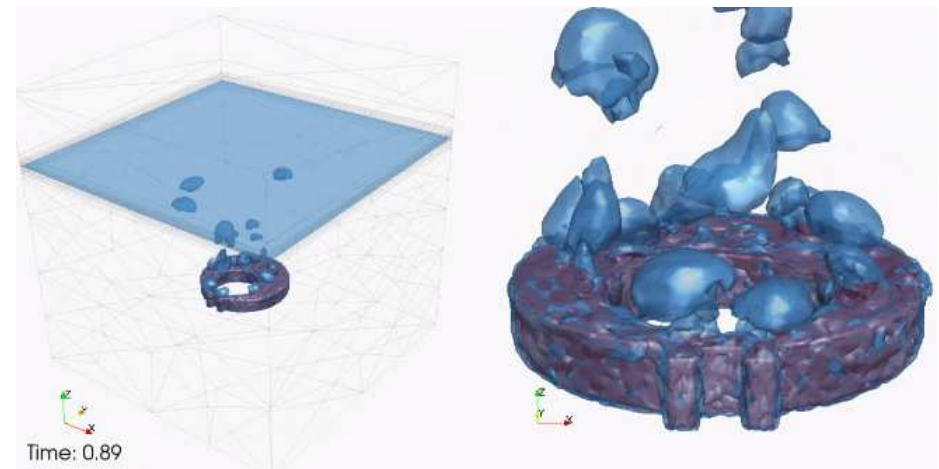
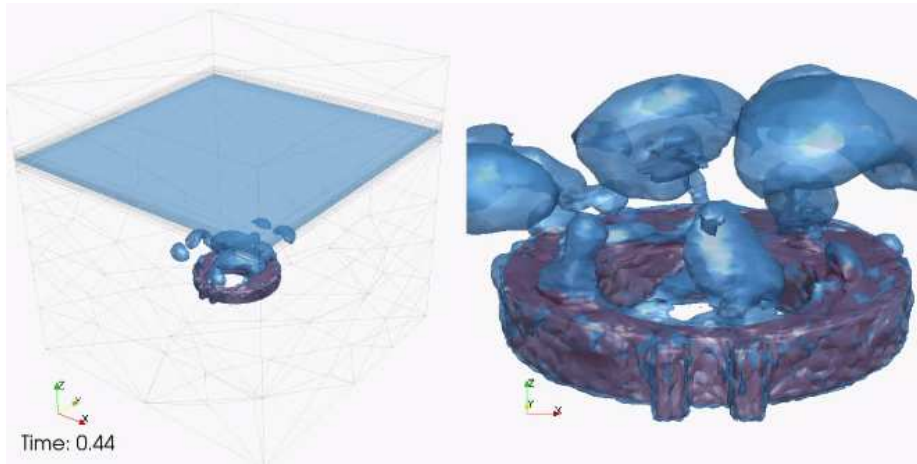


Water level : 0.1m above the vapor  
film  $P=1$ bar

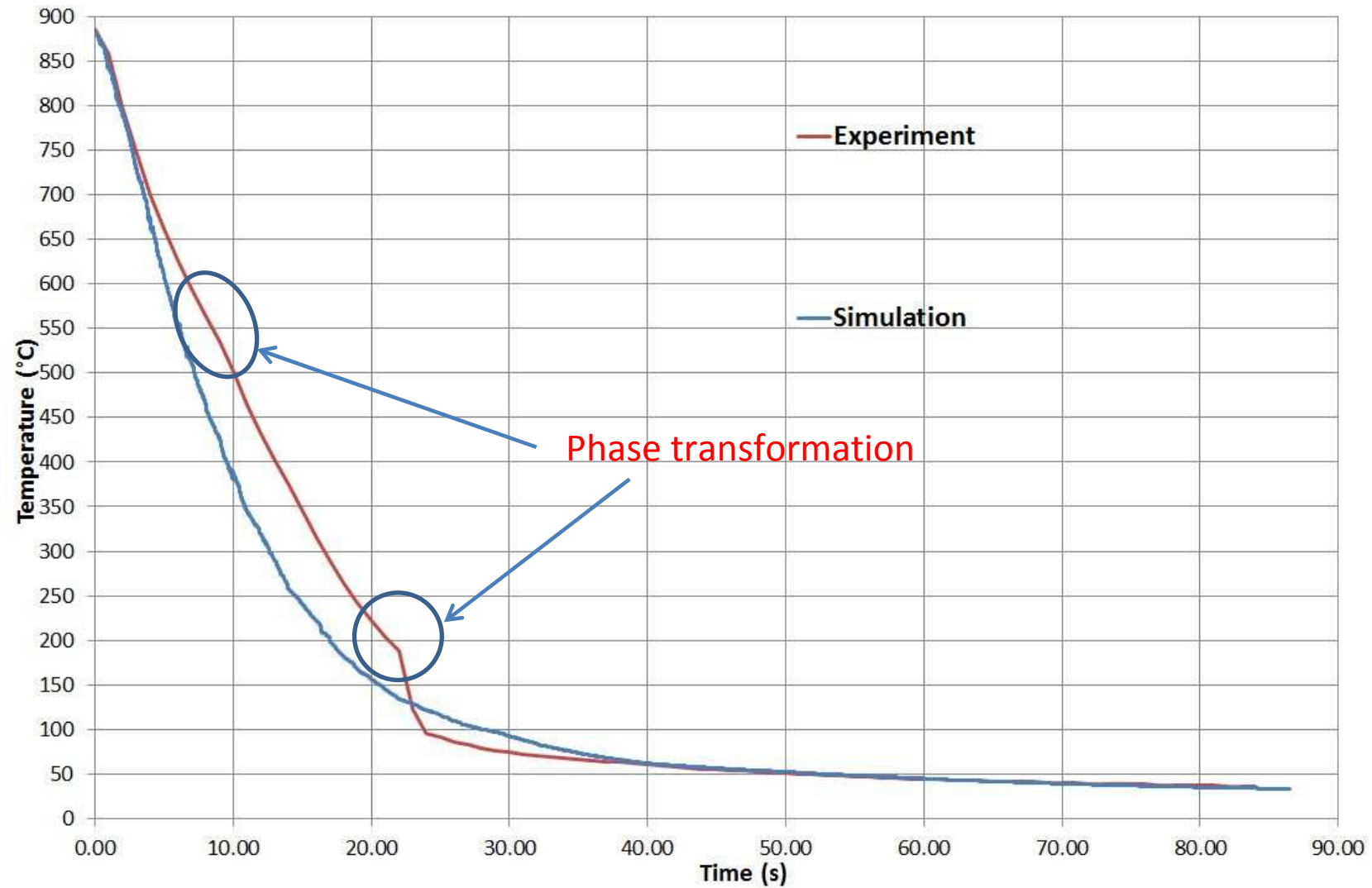
## 6- liquid – gaz – solid flow (2D)



## 6- Industrial Parts



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Evolution of the temperature at the center of the sample

## ■ ■ Conclusion & Perspectives

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- ❑ An Eulerian framework for multiphase flows
  - ❑ Combined with a high fidelity anisotropic mesh adaptation
  - ❑ Variational Multiscale FE Method for turbulent multiphase flows
  - ❑ Implementation of an implicit surface tension and a conservative LS
  - ❑ Towards turbulent boiling and phase change
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- ❑ Conservative interpolation after meshing (phd in progress)
  - ❑ Nonlinear subscales and higher order discretisation (in progress)
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- ❑ Phase change with compressible features
  - ❑ Phase transformation
  - ❑ Wetting and contact angle